

Error Compensation in Flow Meters

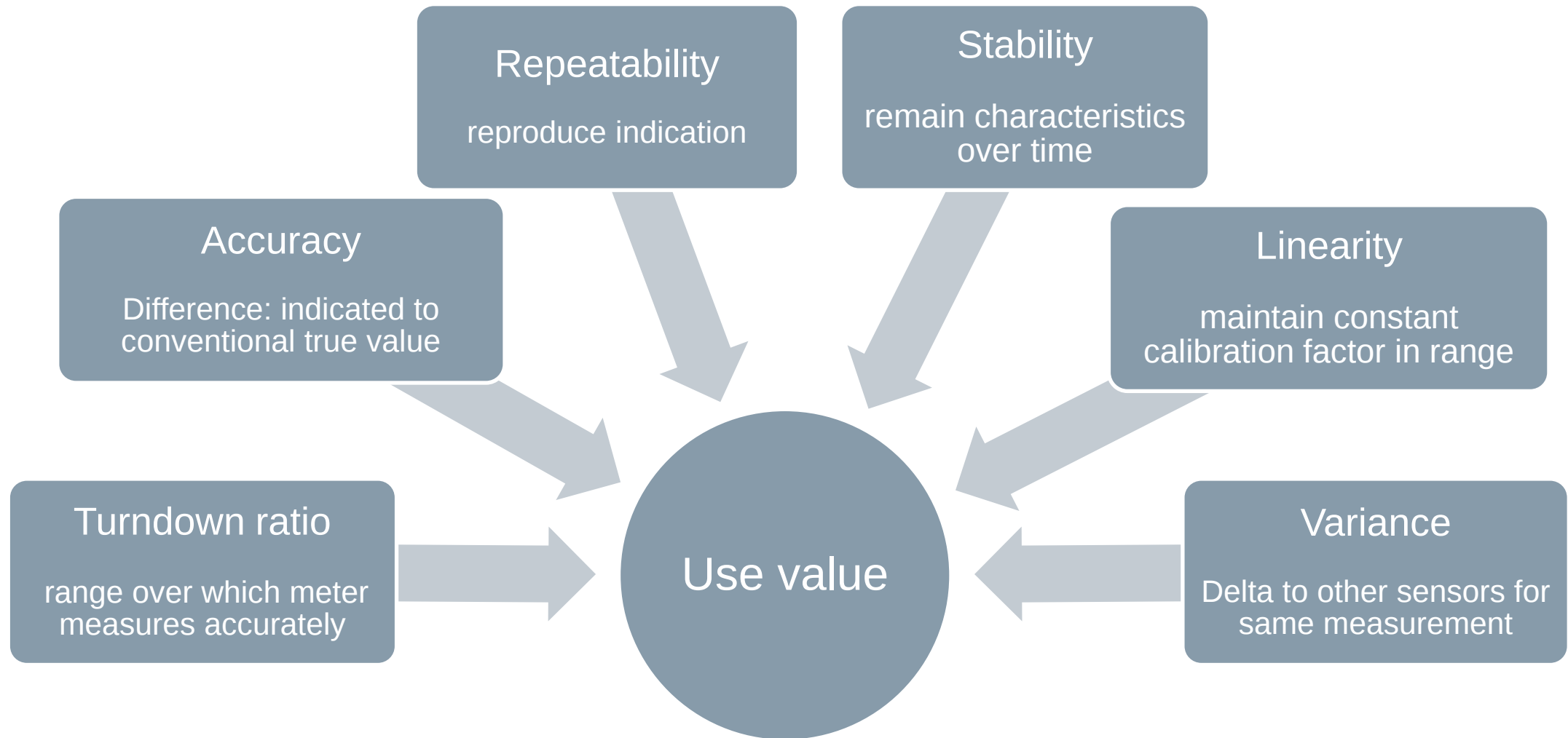
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Objective



- View on competitiveness of flow meters
- Process control versus custody transfer
- Limits of turn-down-ratio
- Complementation of Sensorfront model with empirical model

Use Value Definition



Exchange Value

Dual character

Instrument satisfying a technical need

Product traded in a market

Technology:

Sensor solves technical problem

- Process control
- Custody transfer

Economy:

Production of commodities by means of
commodities

Economic value = $\max \{ \text{price in free market} \}$

Observation

- Growing necessity to minimize overall production costs
- Potential demand from multi-sensor data fusion:
 - less costly sensors
 - compensated by higher numbers of sensors

Indication

Customer's wish

- 1) Buy it - for LOWEST price with acceptable performance/service
(buyers are not necessarily control folk)
- 2) Install it
- 3) Commission it
- 4) Forget it

Compromising certain product requirements

- Base accuracy of high performance mass flow meters $\approx 0.1\%$ (liquids)
- $\approx 70\%$ of mass flow meter market can tolerate base accuracy of 1%
- Control applications focus often on time derivatives instead of absolute values

Cost reduction in

- Software ?
- Hardware ?
- Mechanics



Lower Design Requirements on Sensors
& Error Compensation in Software

Objective of Error Compensation

Minimize:

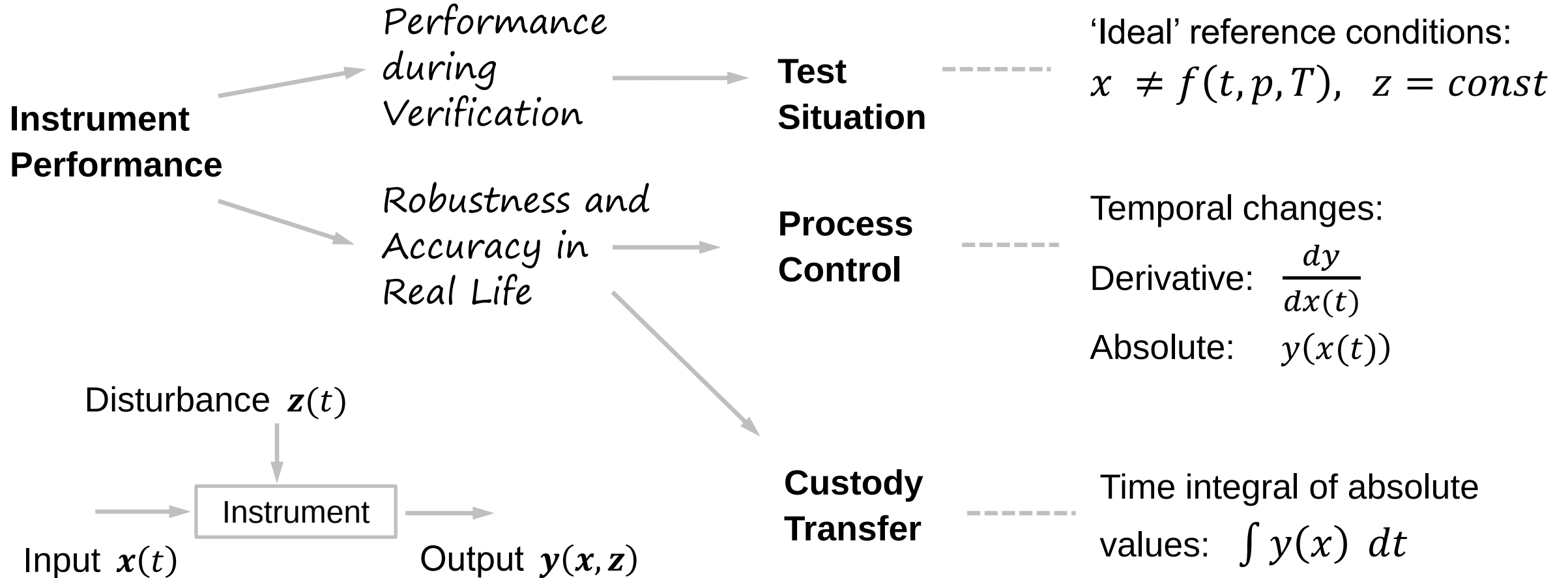
1) Dependency of absolute error on

- Flow rate
- Fluid temperature
- Fluid pressure, etc

2) Dependency of zero flow rate on

- Fluid temperature
- Fluid pressure
- Mechanical stress situation, etc

Differentiation into: Rate of Change, Absolute Value and Integral Value



Mass Flow Meter: Input x , Output y , Disturbance z

Continuous input:

$$x(t) = \{ \dot{m} \} \quad \text{true flow rate}$$

Absolute continuous values:

$$y(t) = \left\{ \begin{array}{l} \dot{m} \\ \rho_{FLUID} \\ (T, p) \end{array} \right\} \quad \begin{array}{l} \text{indicated flow rate} \\ \text{fluid density} \end{array}$$



Main disturbance:

$$z(t) = \left\{ \begin{array}{l} T_{FLUID} \\ p_{FLUID} \\ T_{AMBIENT} \end{array} \right\} \quad \begin{array}{l} \text{fluid temperature} \\ \text{fluid pressure} \\ \text{ambient temperature} \end{array}$$

Time integral over transfer period: $t_1 \rightarrow t_2$

$$y_{12} = \int_{t_1}^{t_2} \dot{m} \, dt \quad \text{transferred mass}$$

A Competitive Product has Low Minimum Flow Rate

- Great turn-down ratio (max-to-min flow rate)
- Overlapping flow rate ranges of nominal product diameters

Max flow rate is limited by pressure drop → Low minimum flow rate

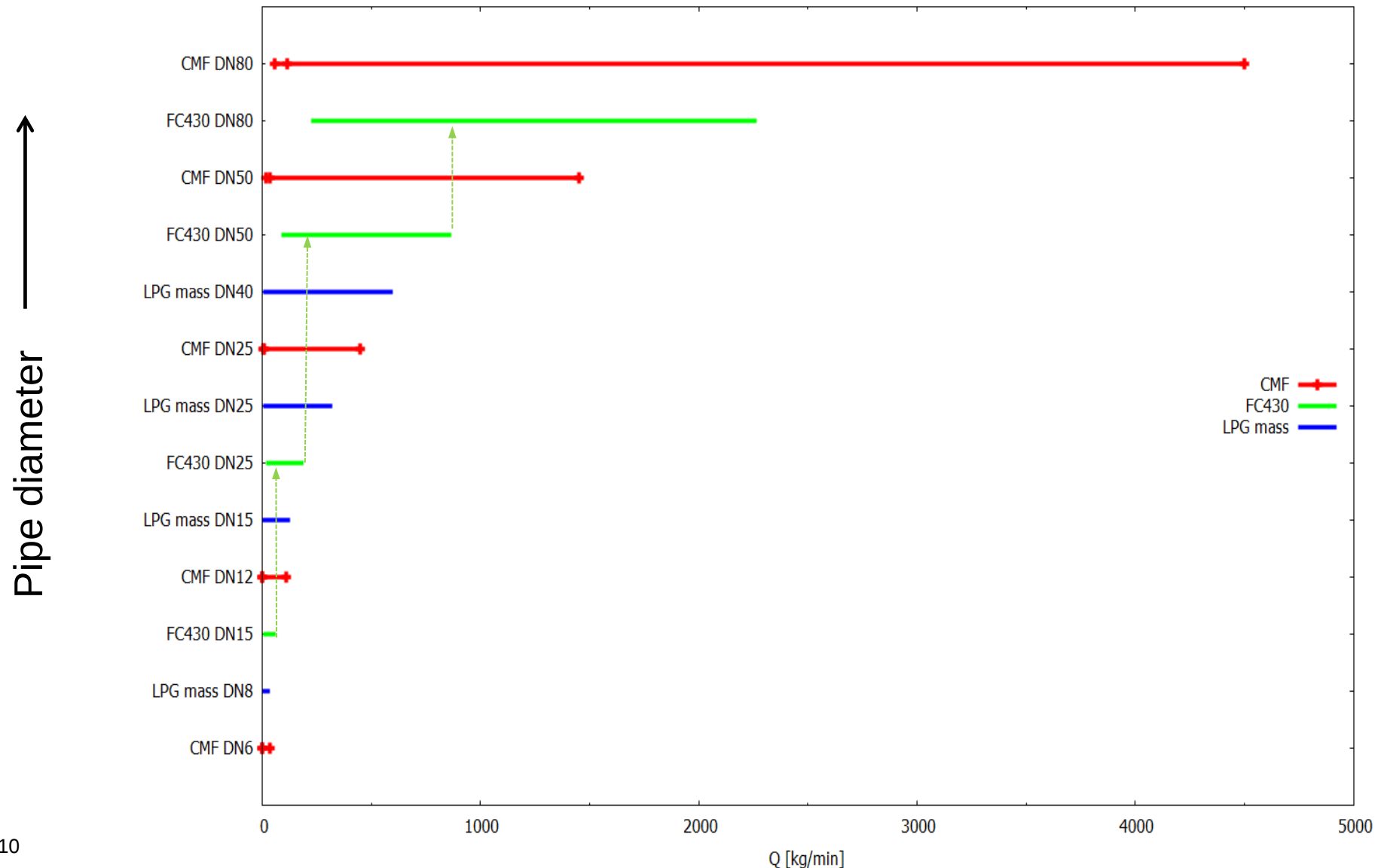


Lower minimum flow rates

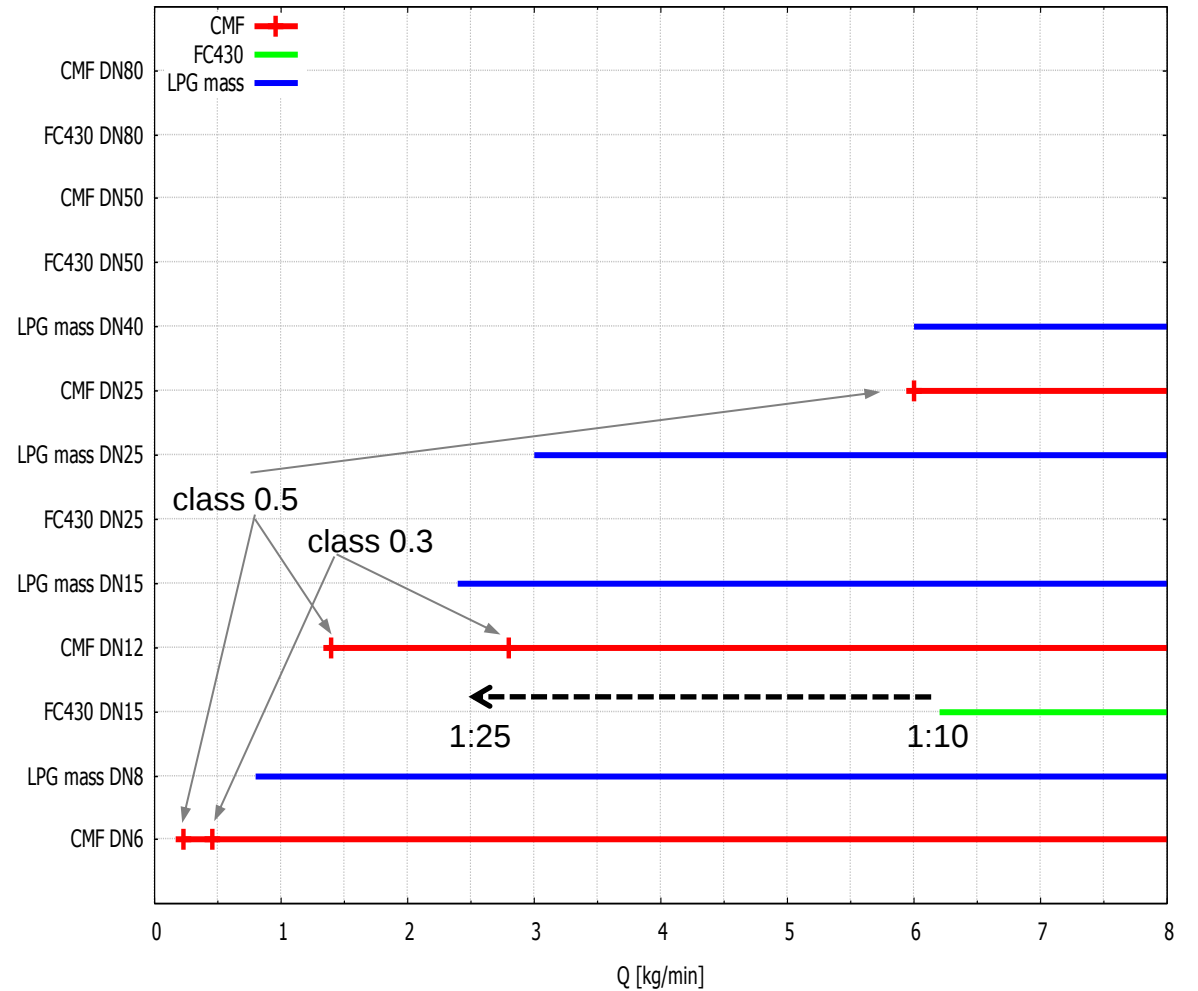
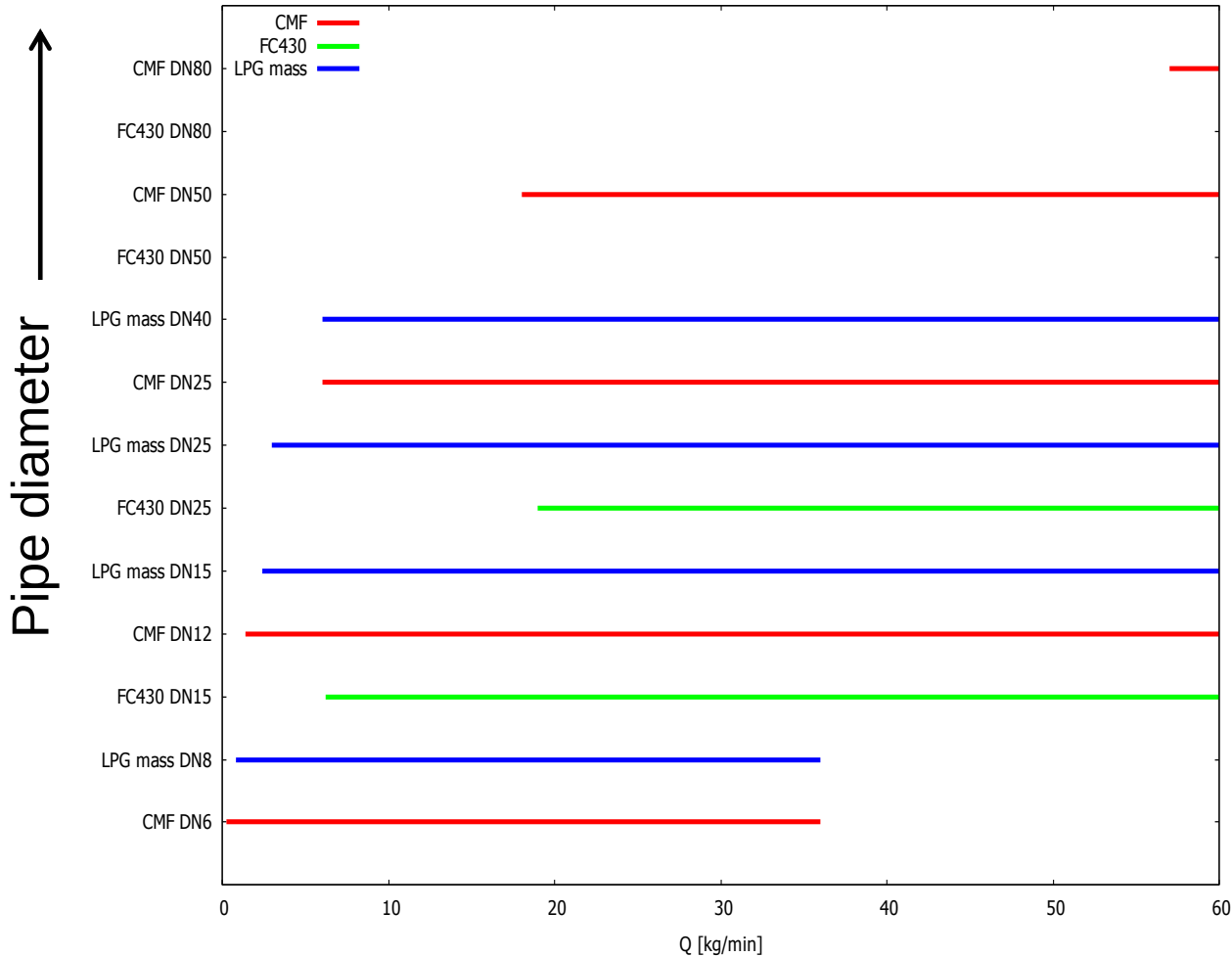
ensuring relative errors less than error limits at:

- Variation of fluid temperature in full operational range
- Variation of fluid pressure in full operational range

Ranges of Mass Flow Rates for different diameters: CMF, FC400, LPG mass

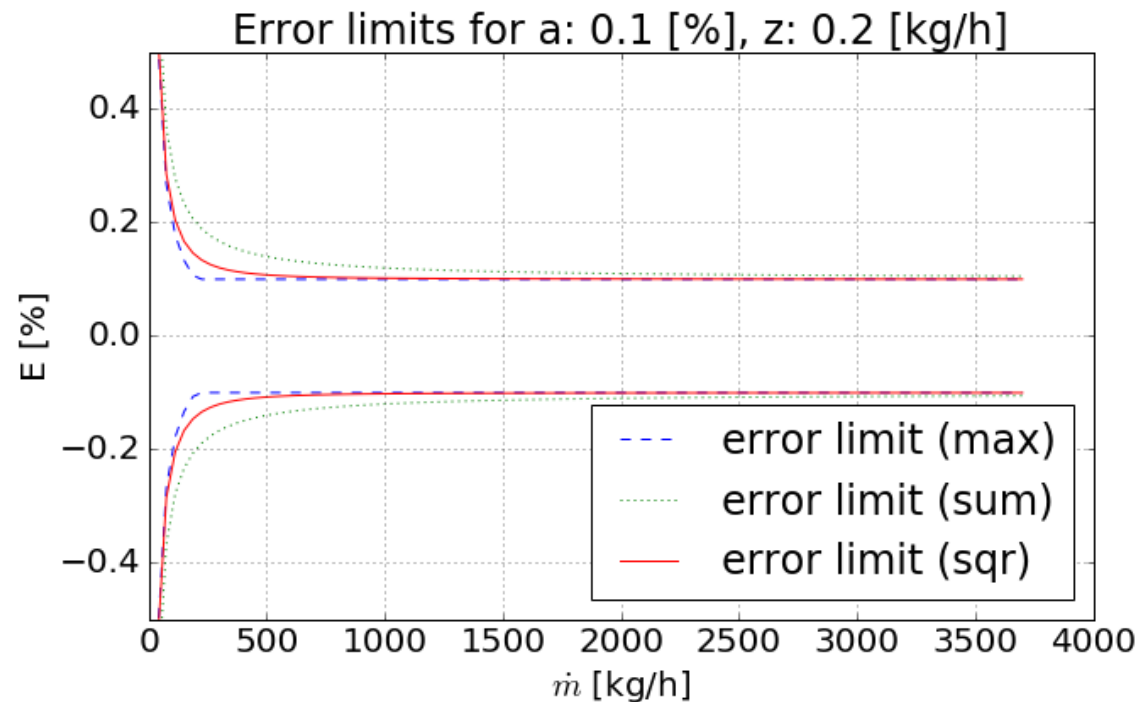


Zoomed: Ranges of Mass Flow Rates: CMF, FC400, LPG mass



What is Limiting the Extension of Turn-down Ratios ?

Limits of relative error, isothermal: $z \neq f(T)$



Error limit E_{lim} :

$$E_{\text{lim}} \geq E = \frac{\dot{m}_{\text{ind}} - \dot{m}_{\text{true}}}{\dot{m}_{\text{true}}}$$

Variants of E_{lim} definition:

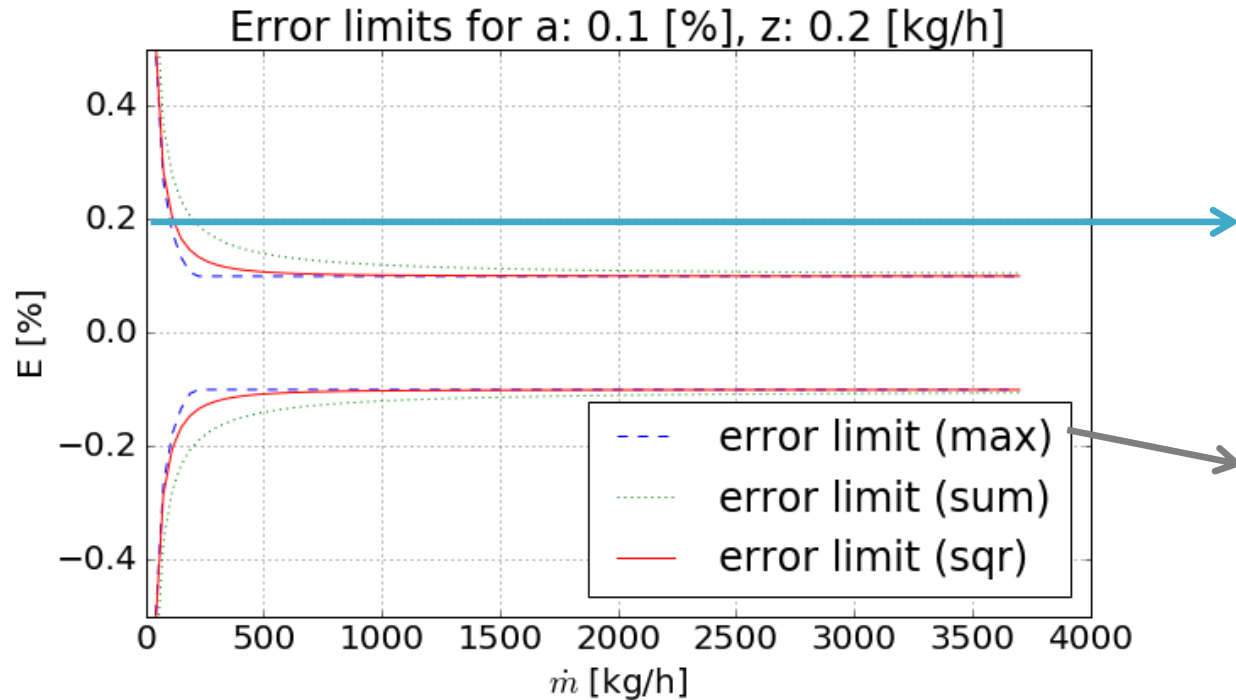
$$E_{\text{max}} = \max\left(a, \frac{z}{\dot{m}}\right)$$

$$E_{\text{sqr}} = \left(a^2 + \left(\frac{z}{\dot{m}}\right)^2\right)^{0.5}$$

$$E_{\text{sum}} = a + \frac{z}{\dot{m}}$$

z .. zero flow error, a .. base accuracy, E .. relative error, $\dot{m}$.. mass flow rate

Error Limit of Product Specification versus Limit of Standard OIML R117



Error limit of OIML standard R117 (0.2%)
independent of flow rate

But error limit of product specification:
dependent on flow rate

OIML Standard R117 : Liquids other than water

The Plan



- a) Increase dynamics of given product or
- b) Reach same dynamics with cheaper mechanical design

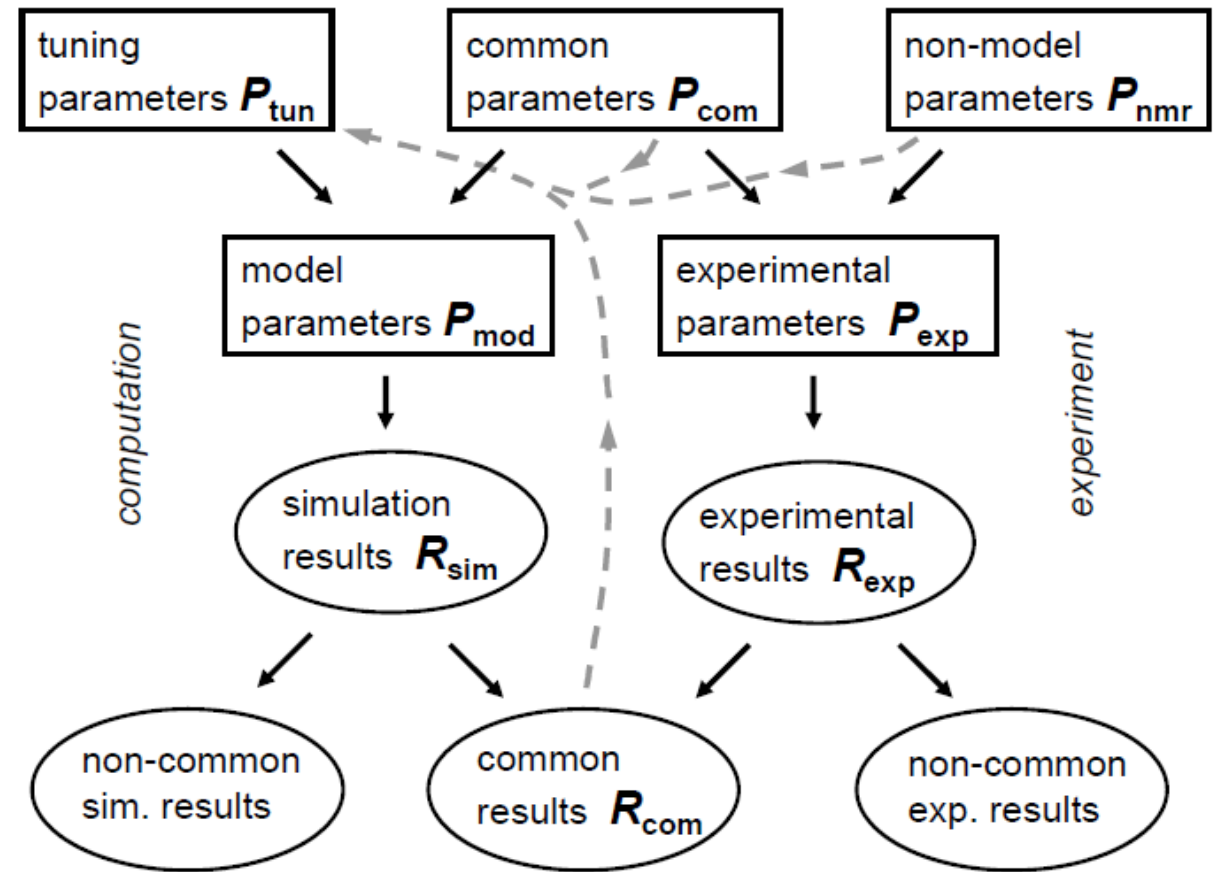
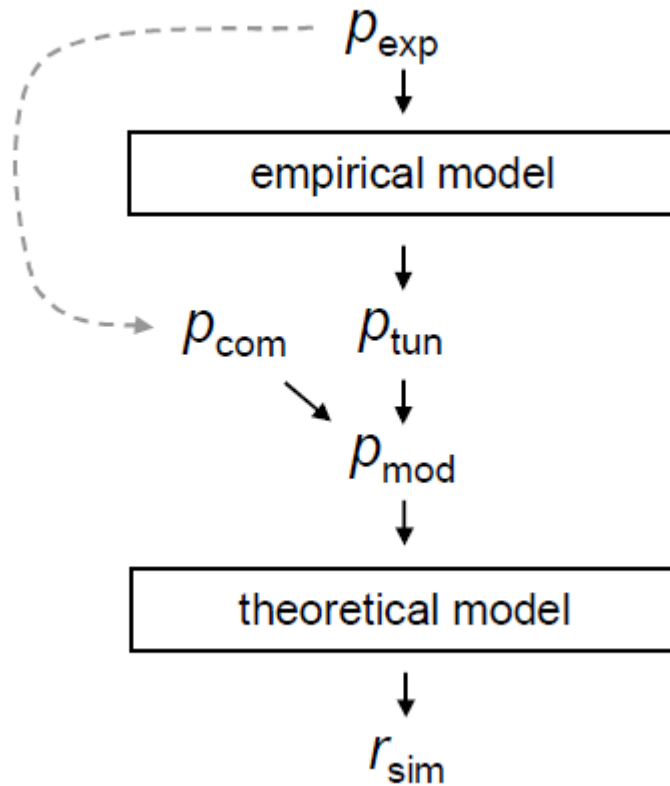
Improving concept of classic calibration

- Offset
- Gain, etc

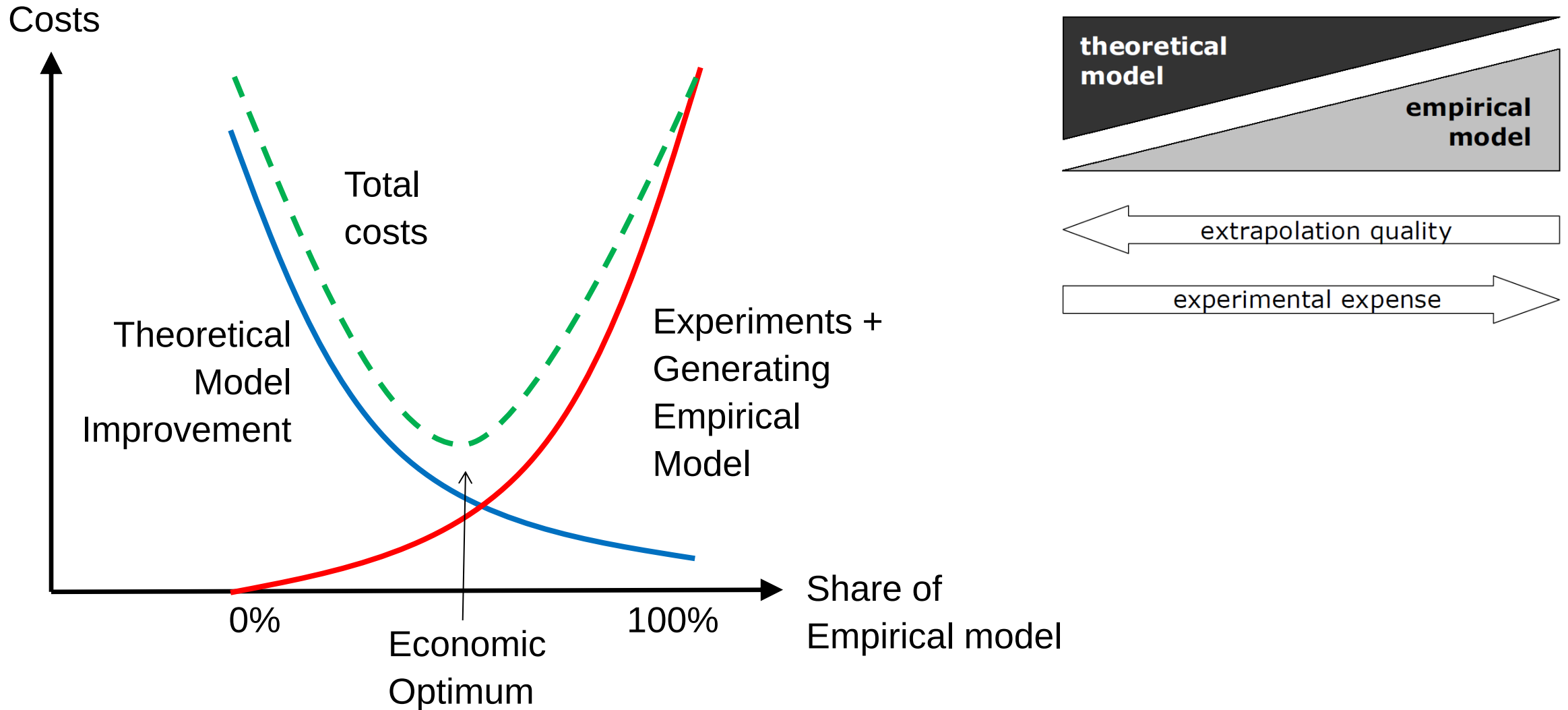
If repeatability is ensured:

- 1) Design tests identifying dependencies
- 2) Approximate absolute and relative error of sensor
- 3) Subtract this error from indicated value

Complement Theoretical Model in Sensor Frontend with Empirical Model



Total Costs versus Empirical Model Share



Improvement of indicated values based either on absolute error A or relative error E (symbols with tilde on top are the approximations)

From theoretical model:

$$A = \dot{m}_{ind} - \dot{m}_{true} \quad \begin{array}{l} \swarrow \text{Reference} \\ \searrow \text{Meter under test} \end{array}$$
$$\dot{m}_{true} = \dot{m}_{ind} - A$$

$$E = \frac{A}{\dot{m}_{true}} = \frac{\dot{m}_{ind} - \dot{m}_{true}}{\dot{m}_{true}}$$

$$\dot{m}_{true} = \frac{\dot{m}_{ind}}{E+1}$$

$\tilde{A}$ and $\tilde{E}$ are functions of disturbances (pressure, temperature) and flow rate

Approximation from empirical model:

$$\tilde{w} = \text{train}(z, \dot{m}_{true}, A) \quad A = \dot{m}_{ind} - \dot{m}_{true}$$

$$\tilde{\dot{m}}_{true}(z, \dot{m}_{ind}) = \dot{m}_{ind} - \tilde{A}(z, \dot{m}_{ind}, \tilde{w})$$

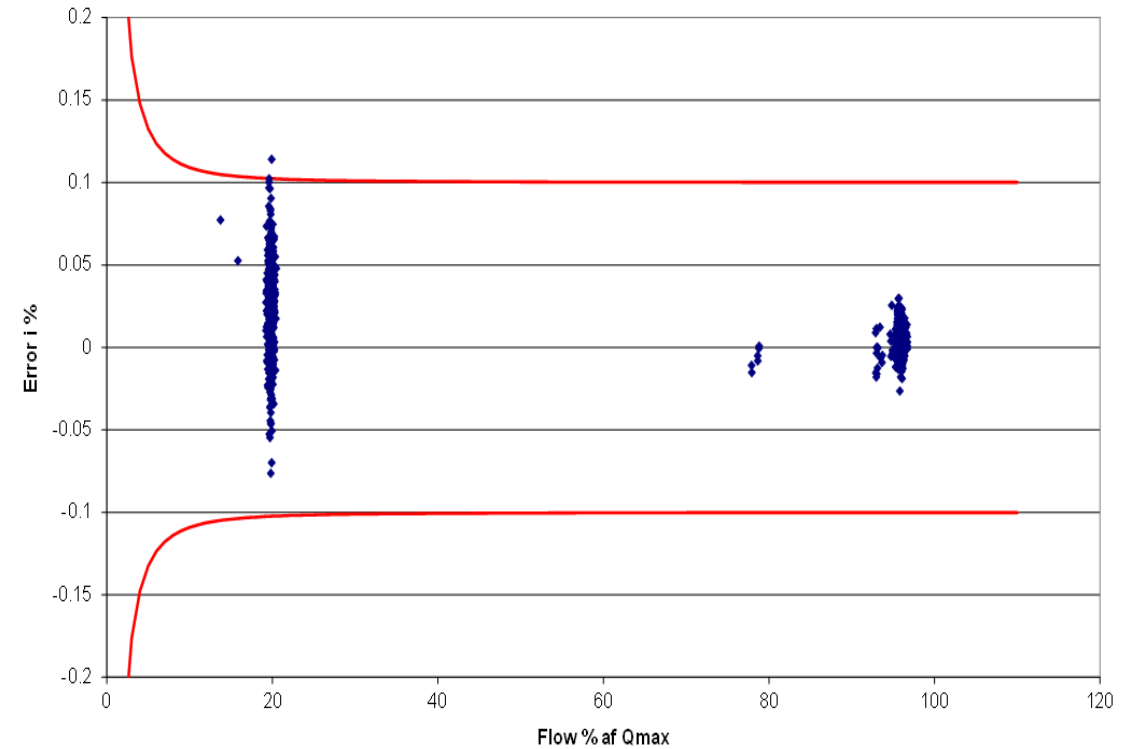
$$\tilde{E} = \frac{\dot{m}_{ind} - \tilde{\dot{m}}_{true}}{\tilde{\dot{m}}_{true}}$$

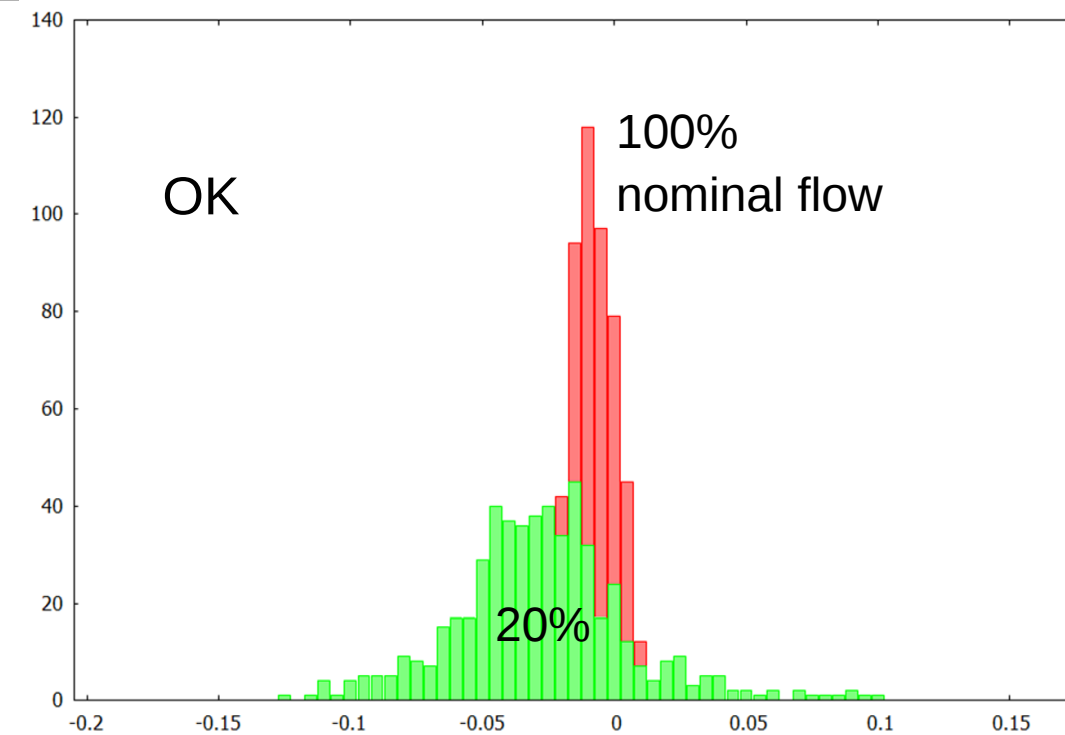
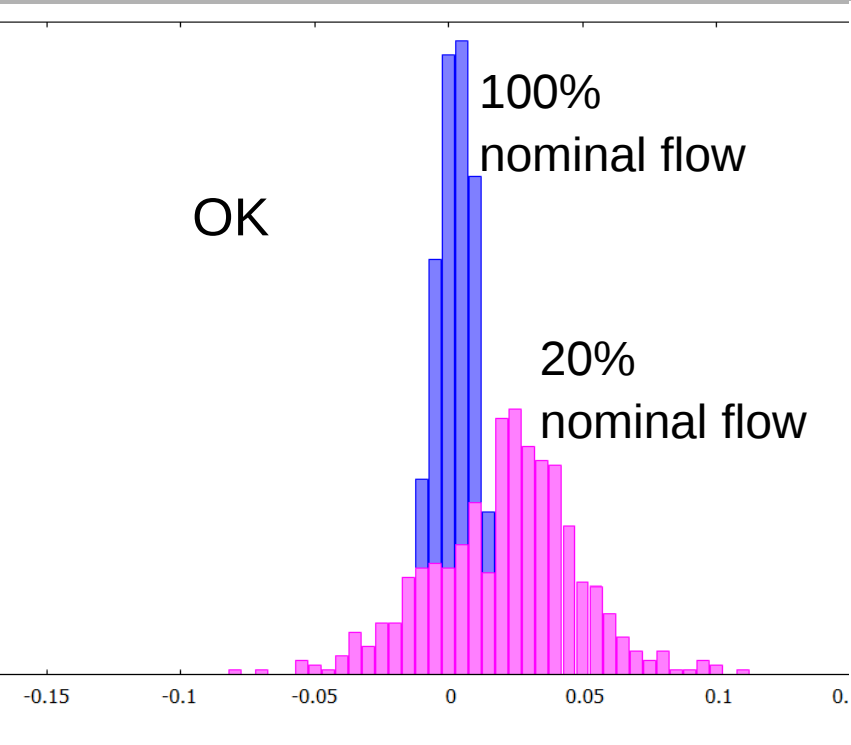
$$\tilde{\dot{m}}_{true} = \frac{\dot{m}_{ind}}{\tilde{E}+1}$$

$$E = \frac{\dot{m}_{ind} - \tilde{\dot{m}}_{ind} - \tilde{A}}{\tilde{\dot{m}}_{ind} - \tilde{A}} = \frac{-\tilde{A}}{\tilde{\dot{m}}_{ind} - \tilde{A}}$$

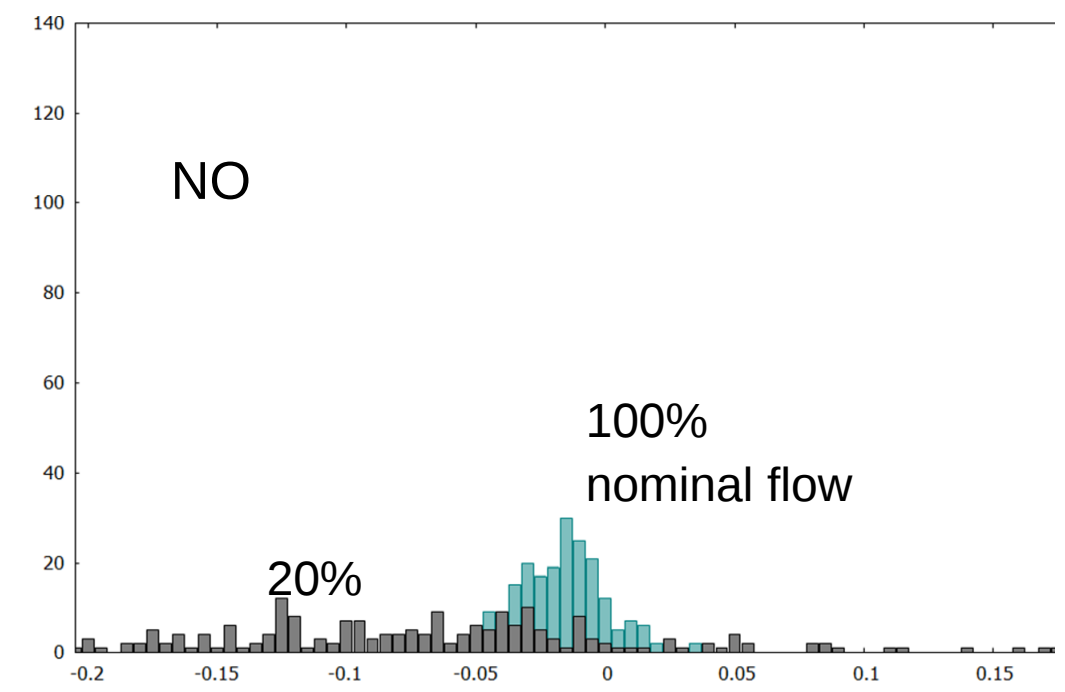
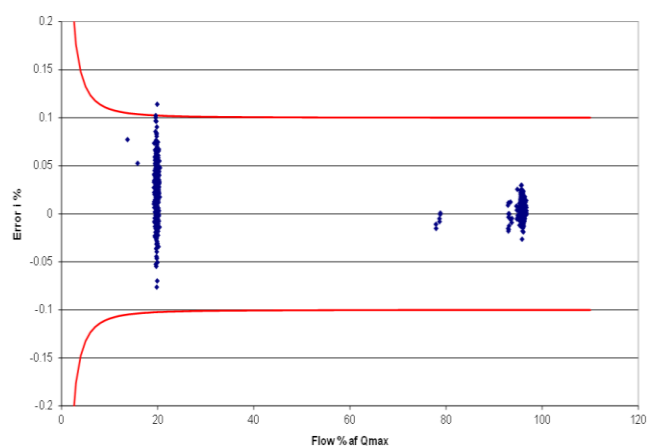
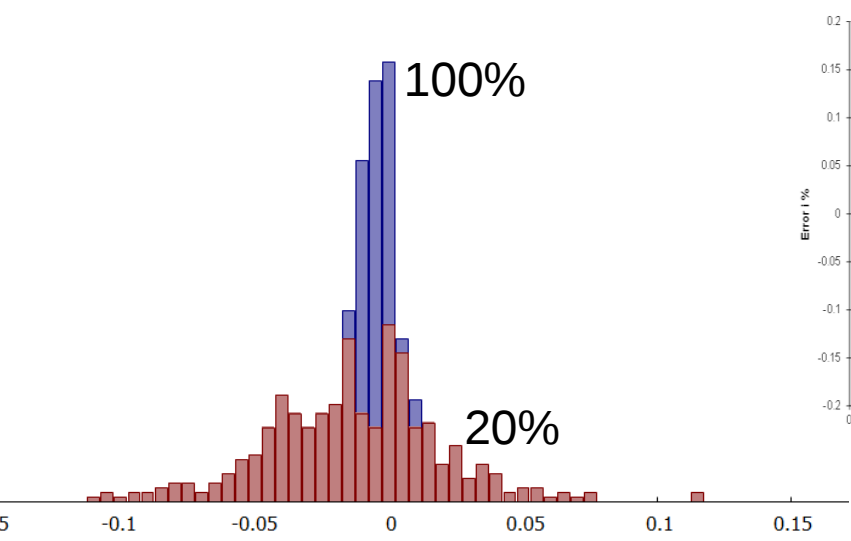
Pre-Requisite:

- Deterministic Behaviour
- Experimental data should be normally distributed
- Chaotic behaviour cannot be compensated

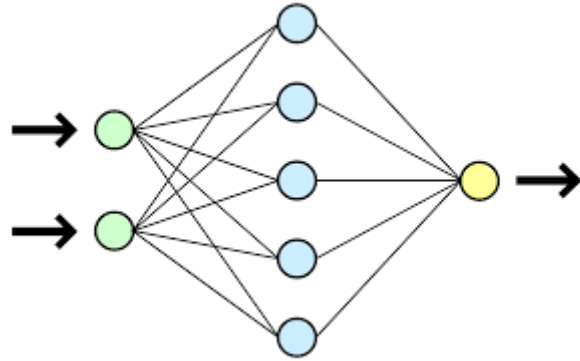




Depends



First Trial: Pure Empirical Model



$$E = f(Q)$$

$$E = f(Q, p)$$

Example:

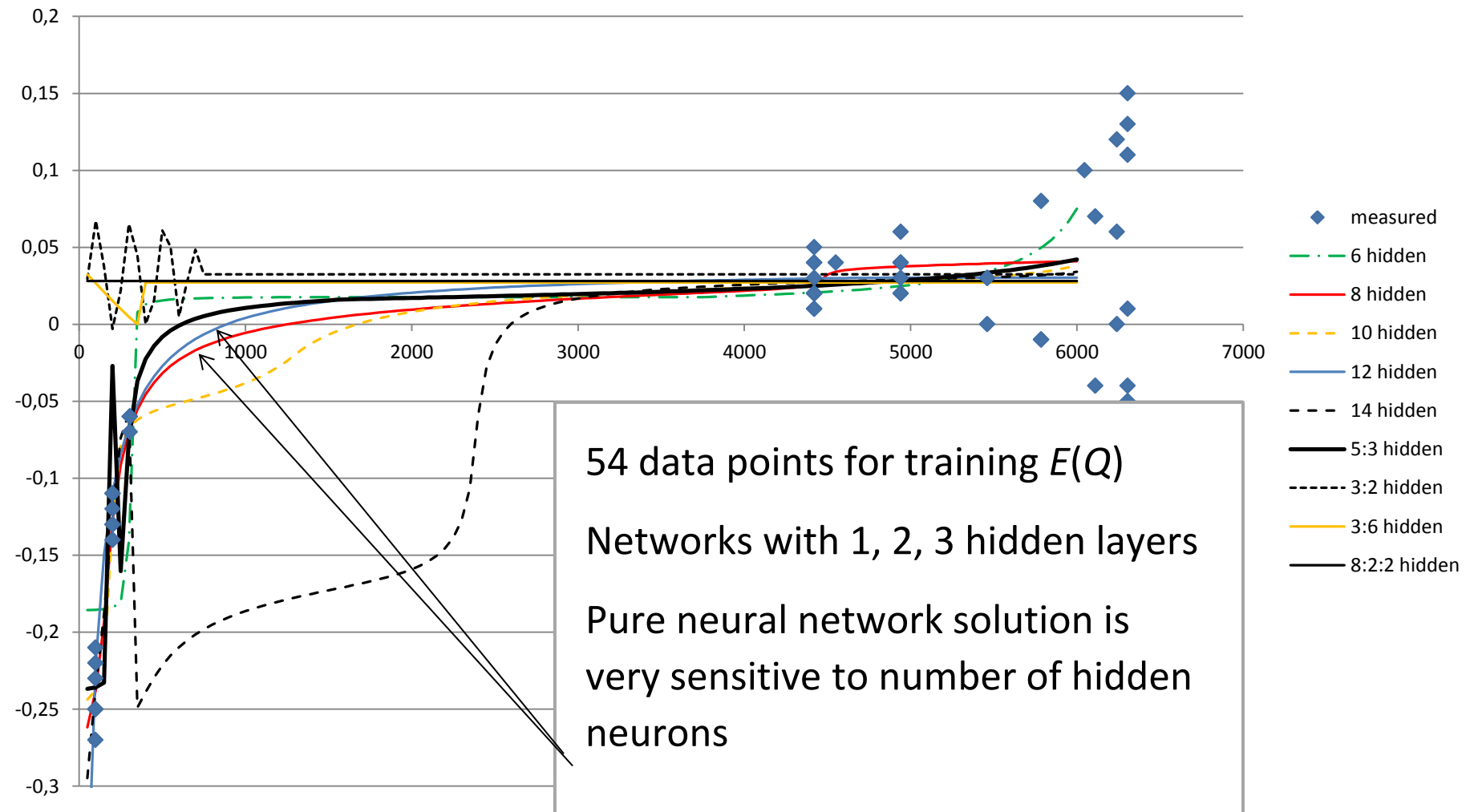
Unusual fluid in food industry
Coriolis meter

Training of model with

x = mass flow rate in [kg/h]

y = relative error in [%]

First Disappointment: Result Sensitive to Neural Net Structure → No-Go

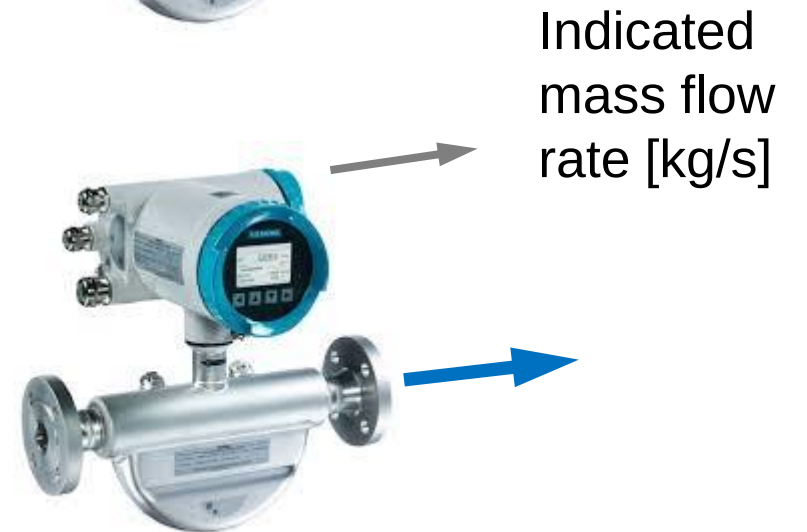


Example: Correction of Error due to Fluid Pressure

Indicated Mass Flow Rate ↔ Zero Mass Flow Rate



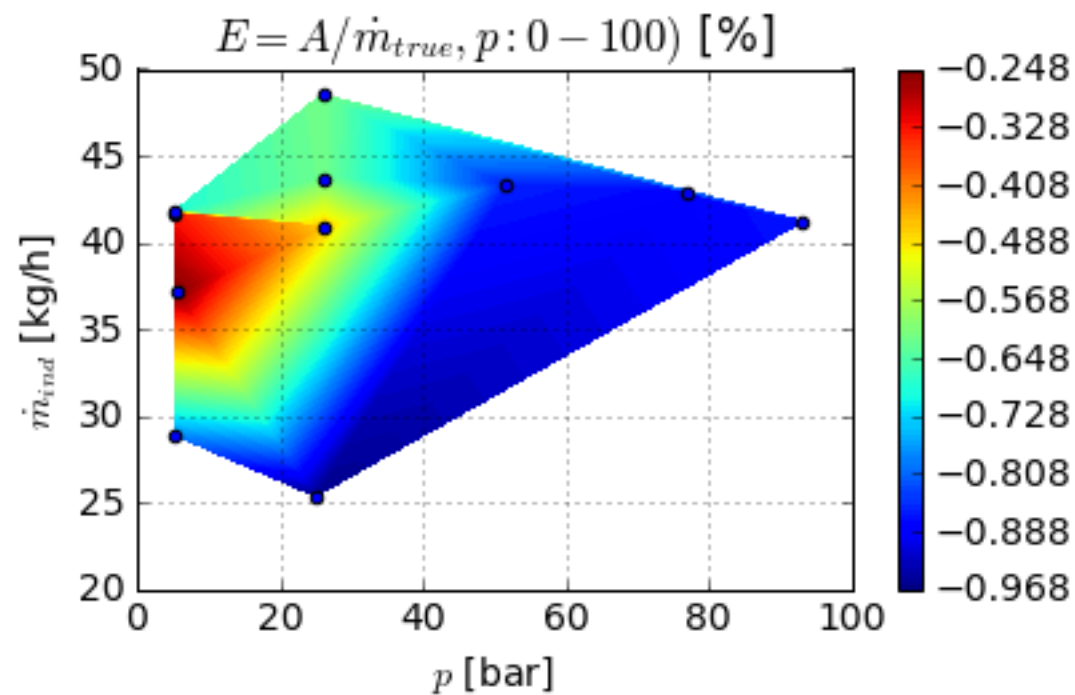
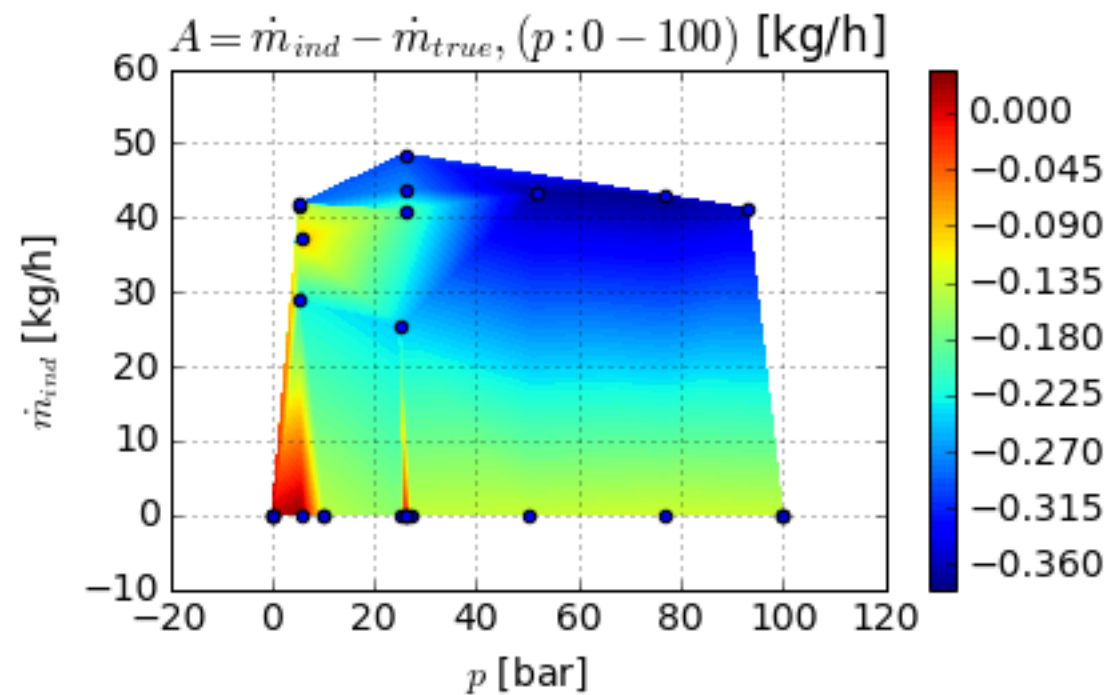
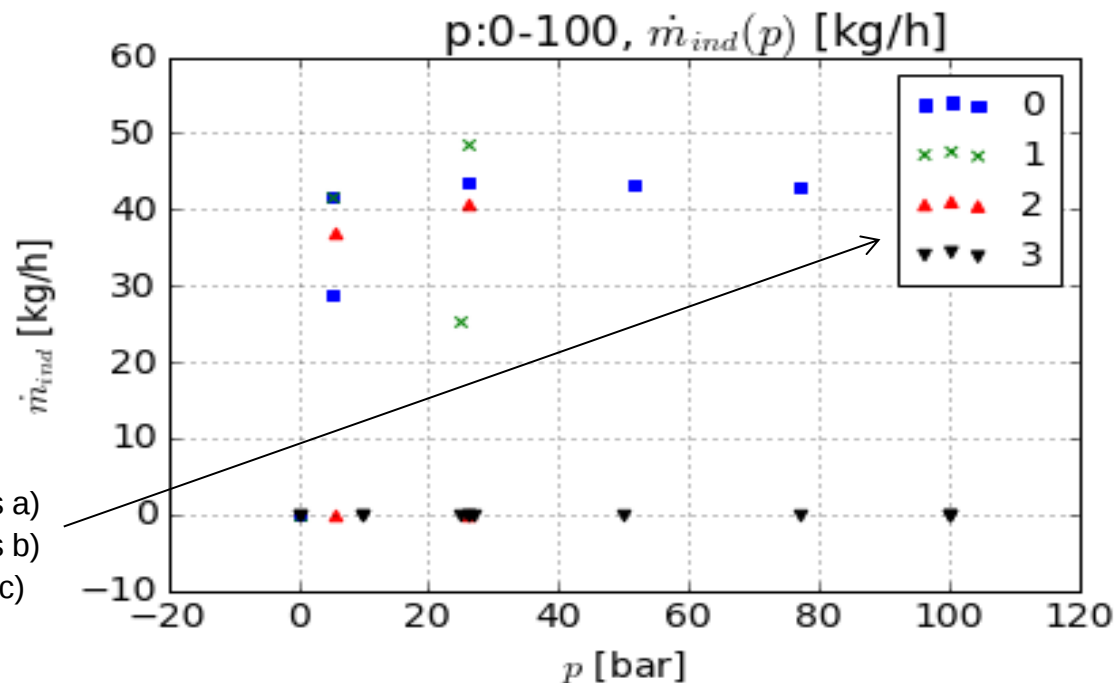
No flow



Conventional
true mass flow
rate [kg/s]

Meter 1: Errors of indicated data,
 A : absolute error [kg/h], E : relative err. [%]

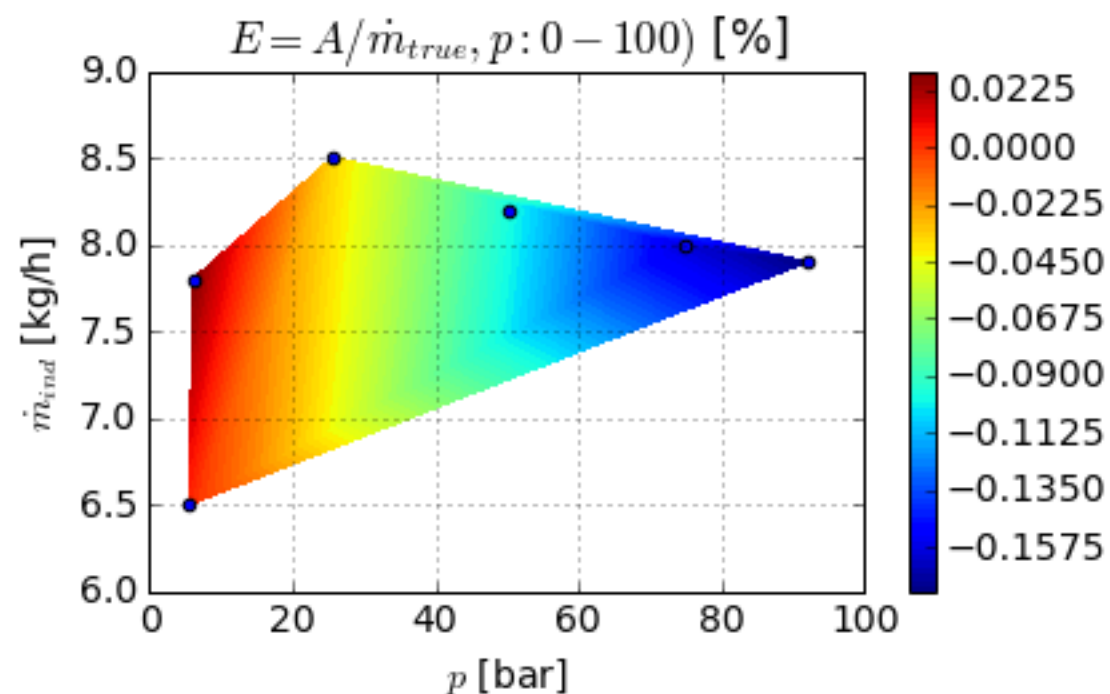
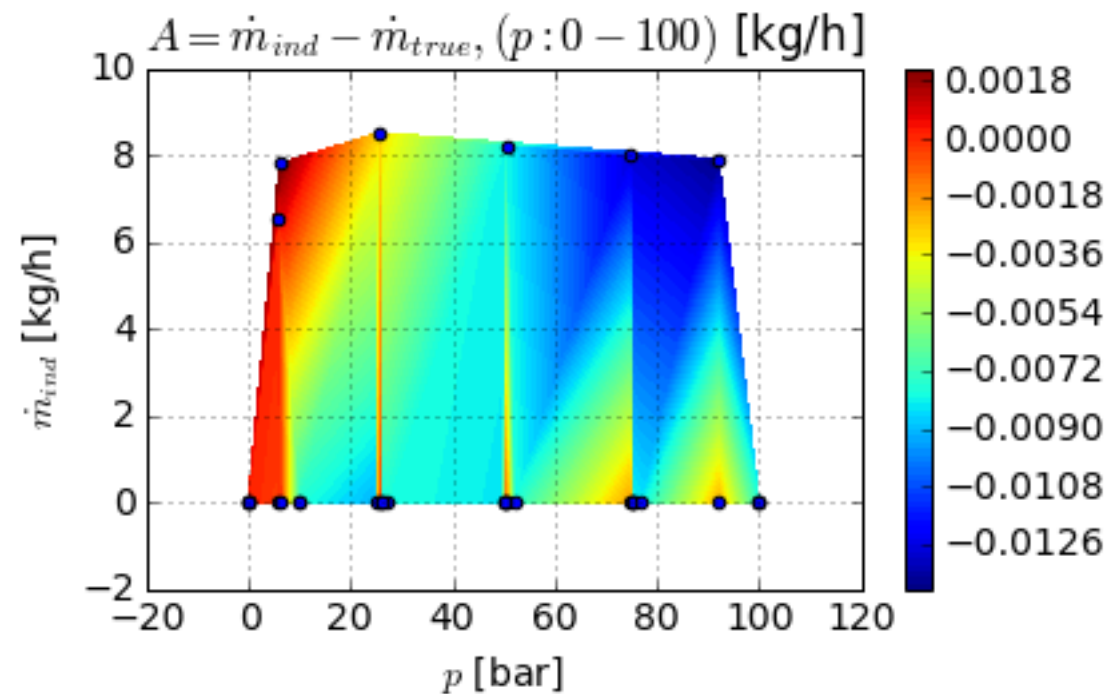
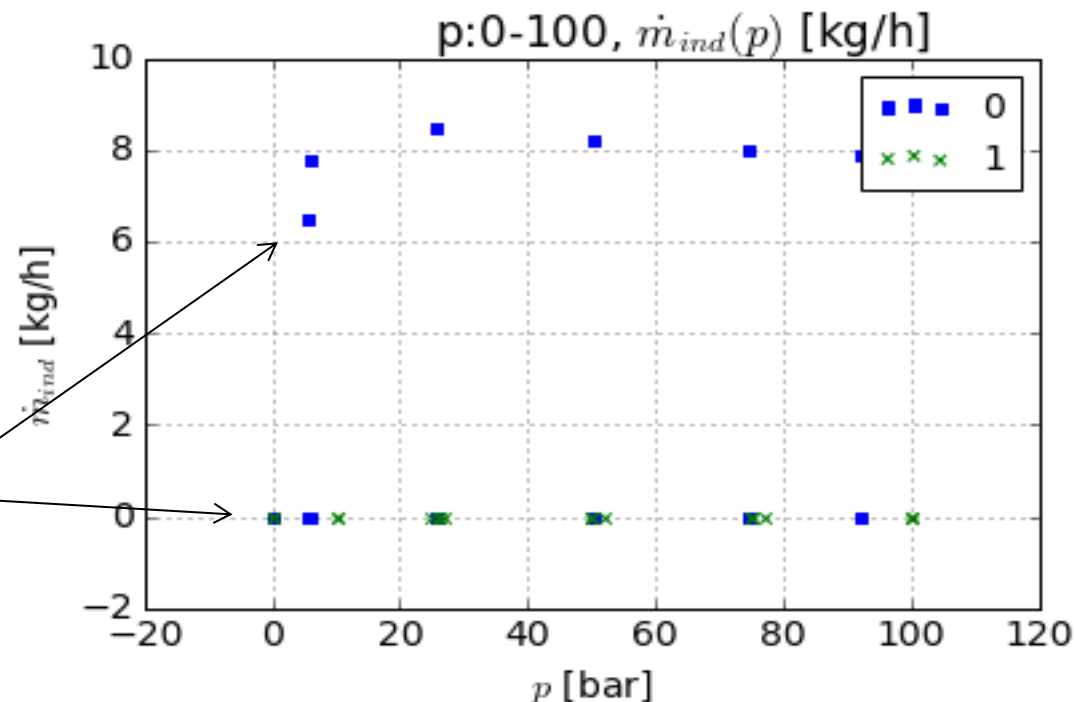
- 0: Original test
- 1: Additional tests a)
- 2: Additional tests b)
- 3: Zero flow (static)

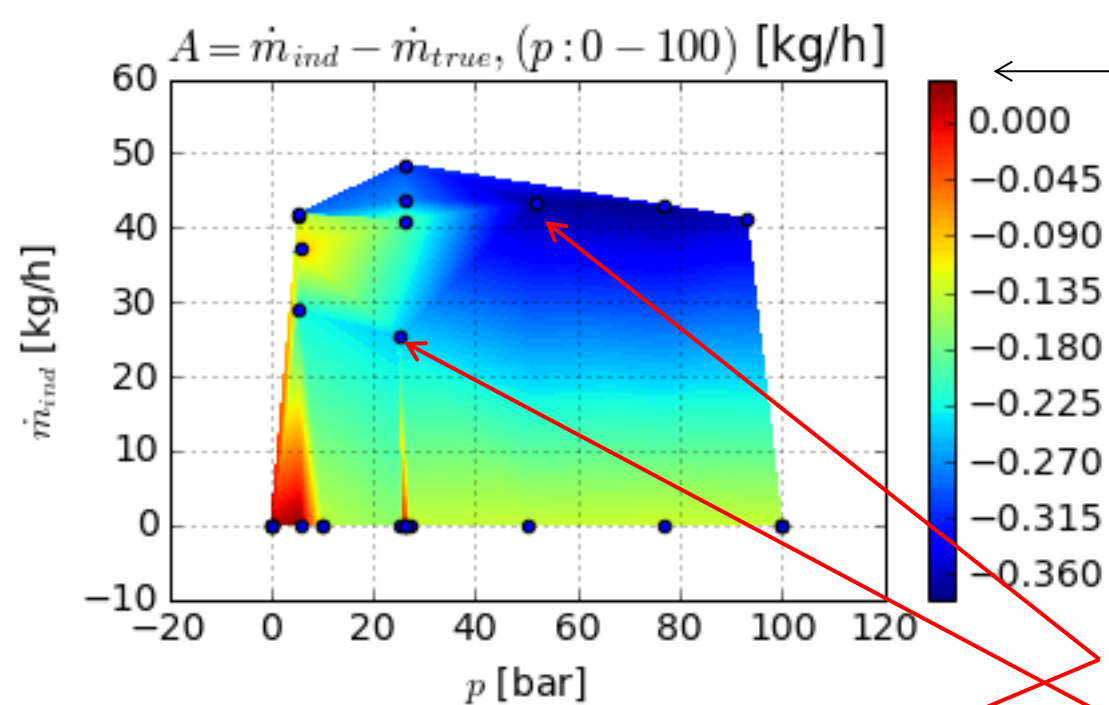


Meter 2: Errors of indicated data,
 A : absolute error [kg/h], E : relative err. [%]

0: Flow tests

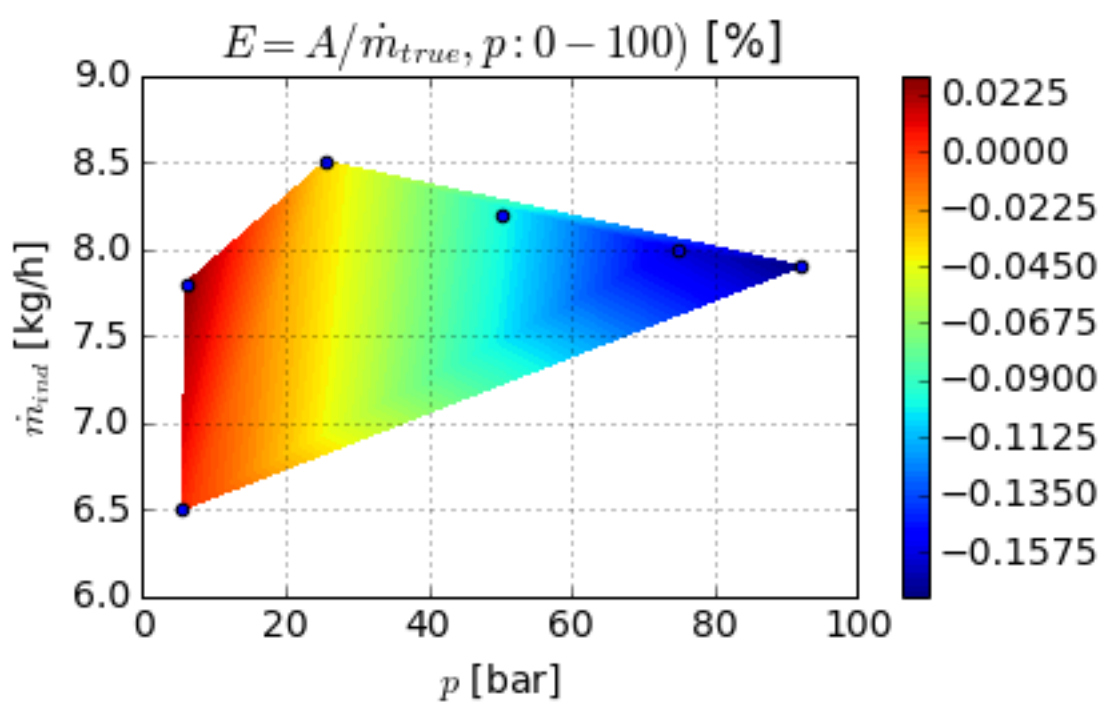
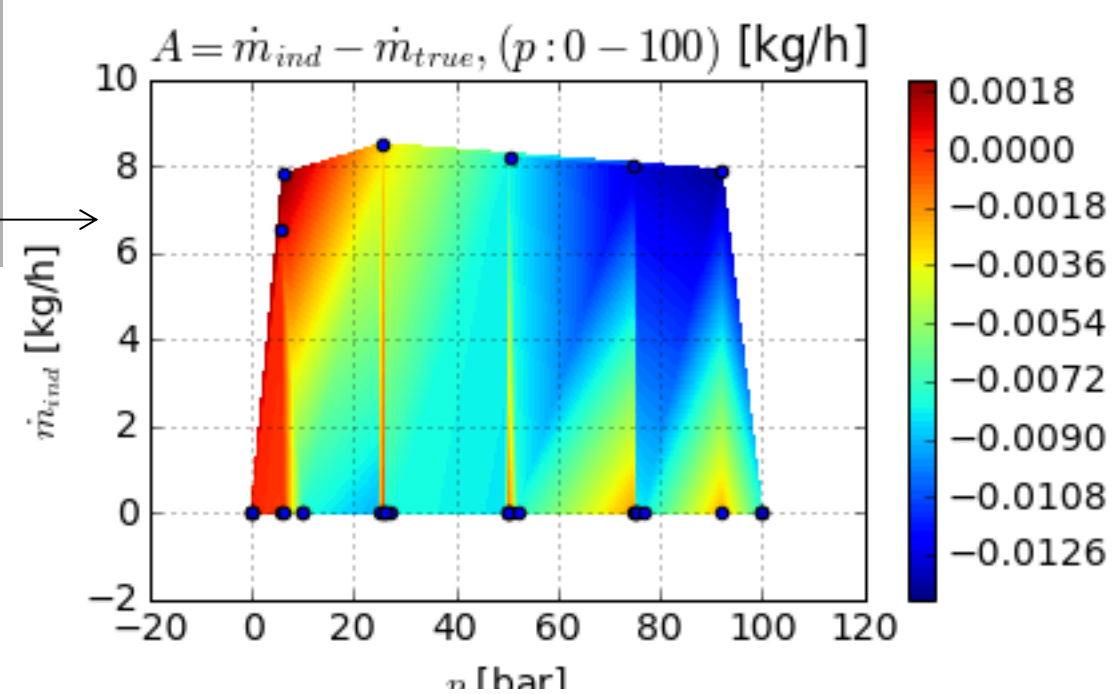
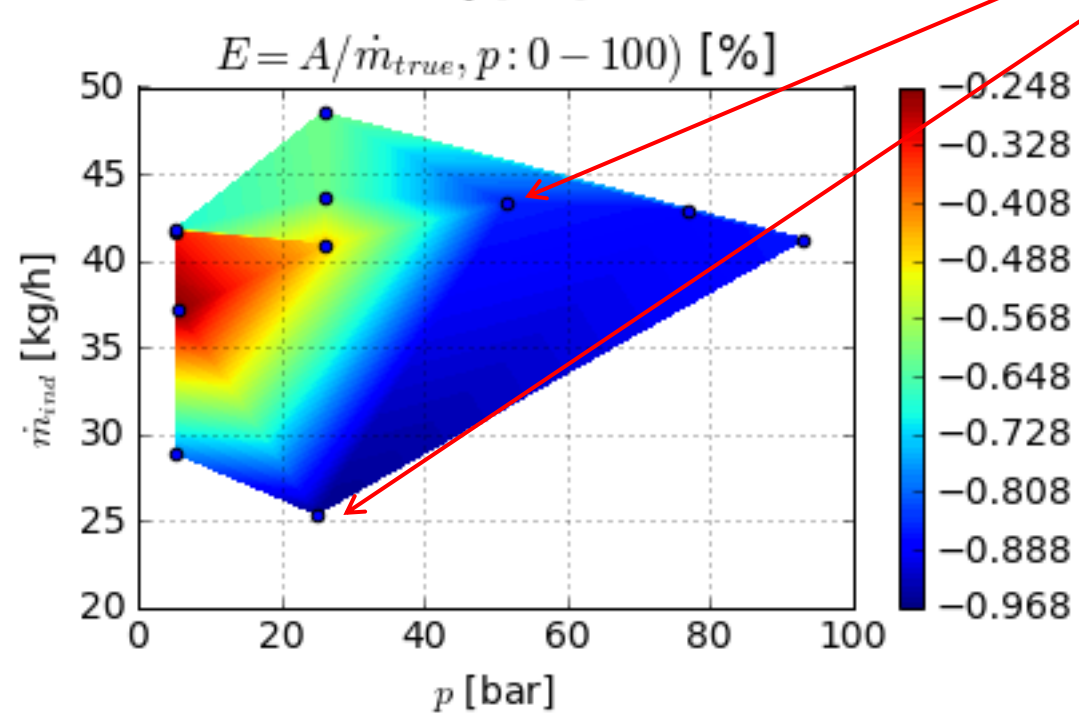
1: Zero flow (static)



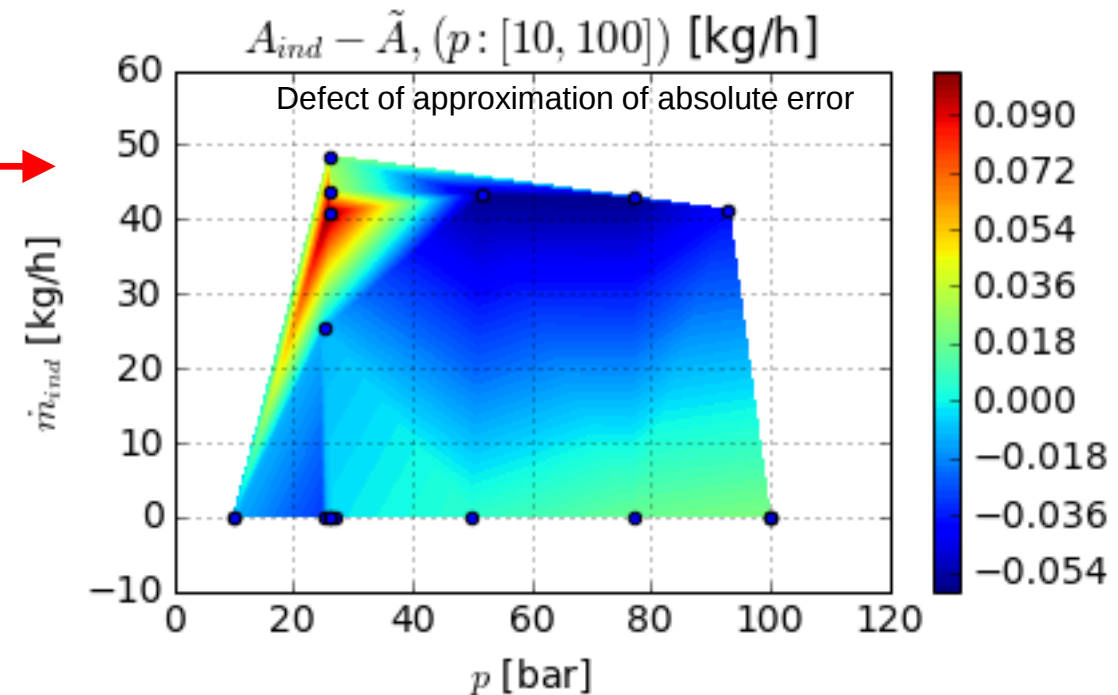
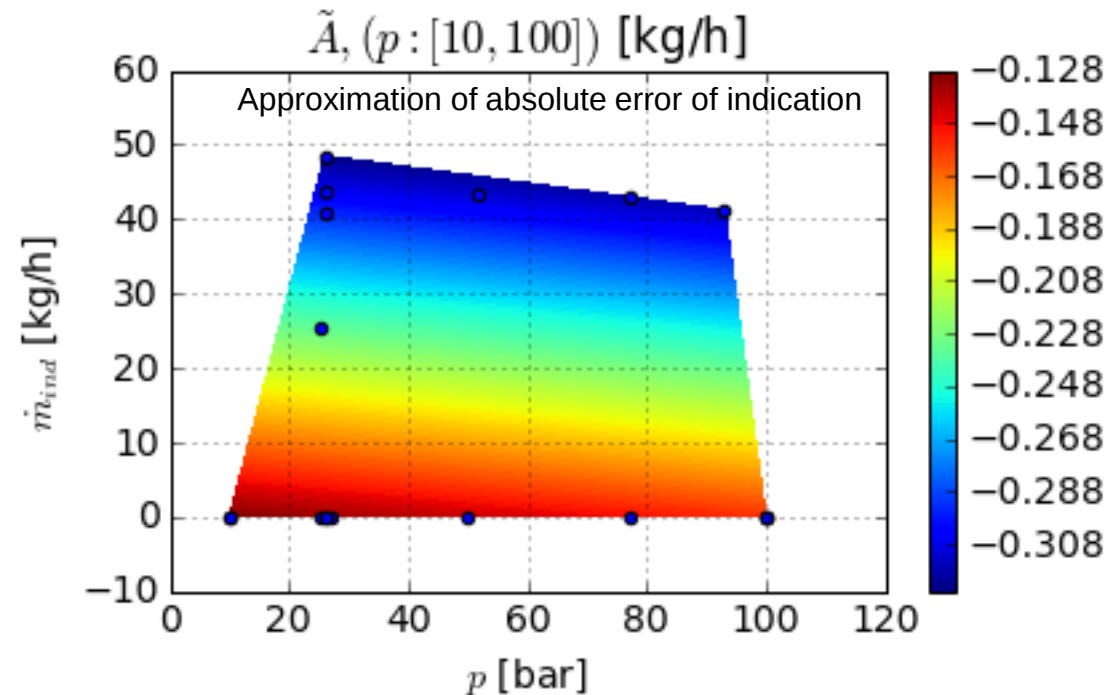
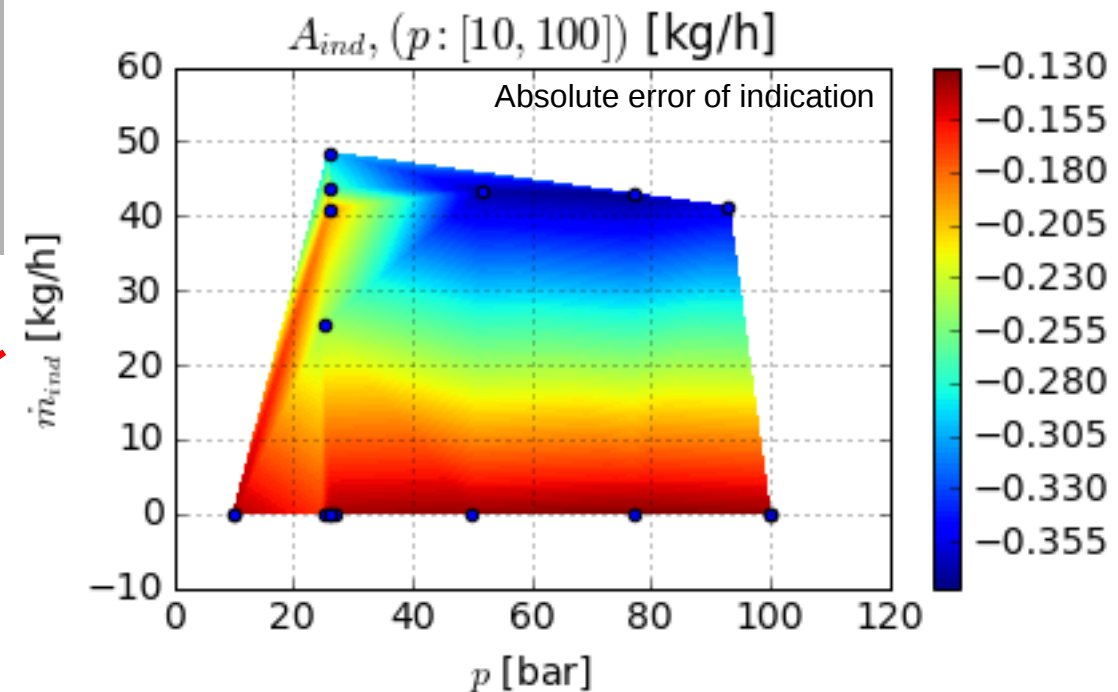


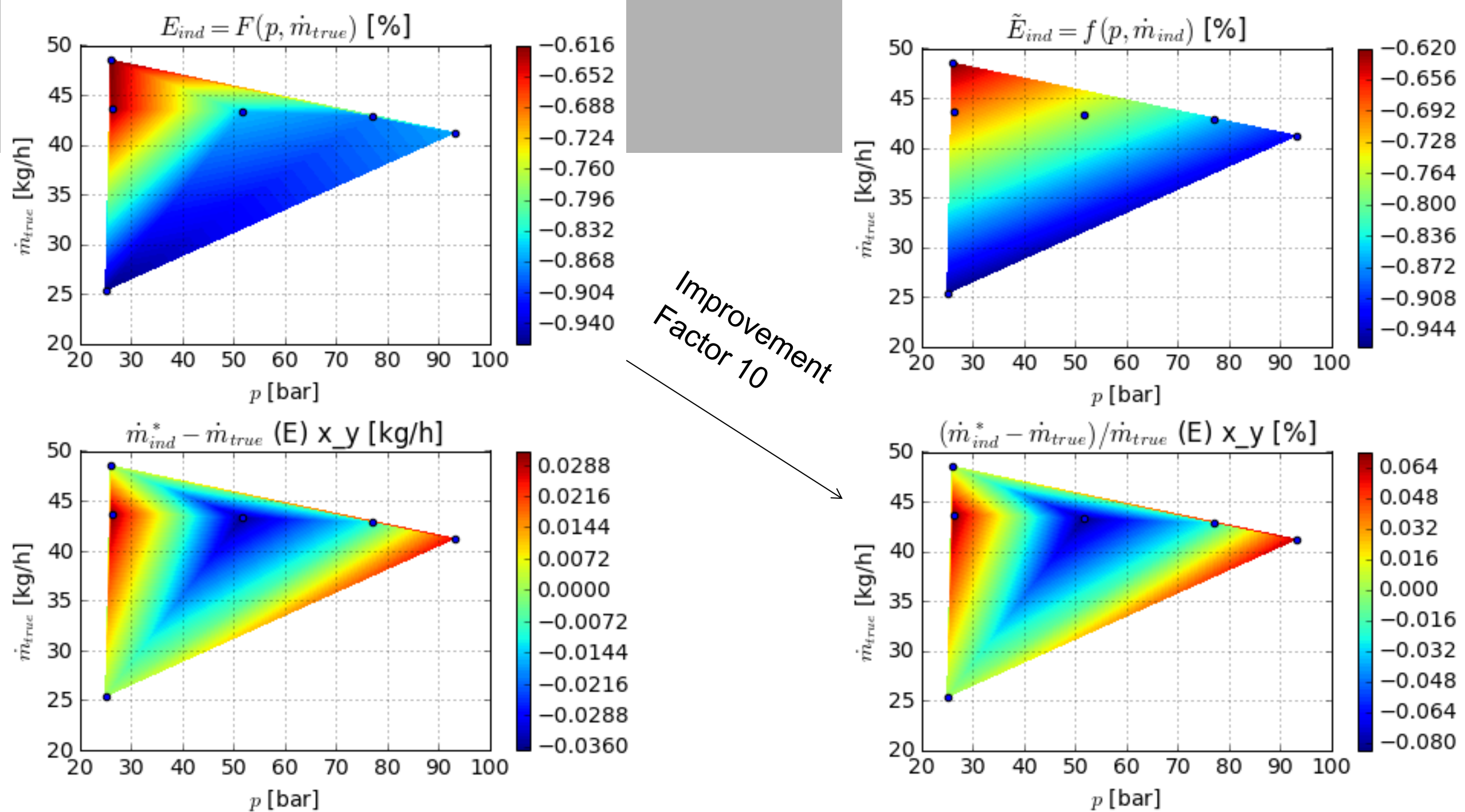
Meter 1

Meter 2

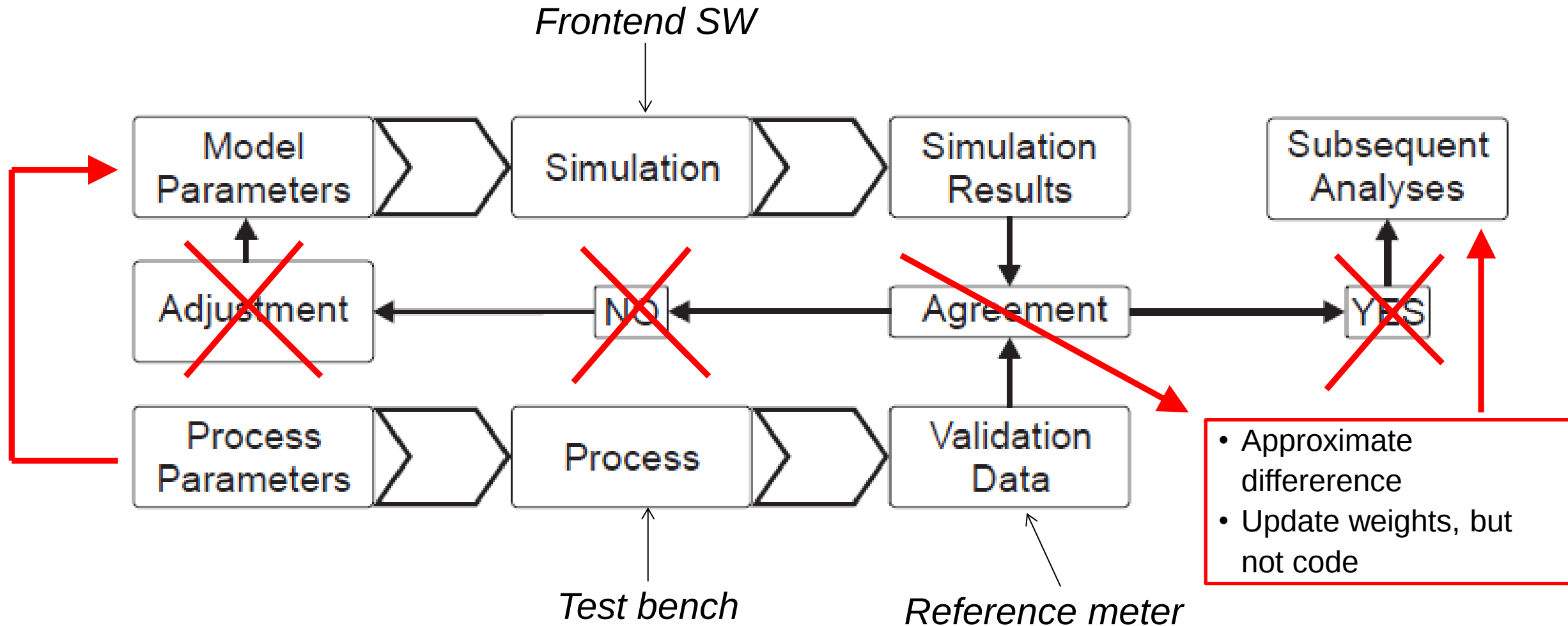


Meter 1: Absolute Error A_{ind} , Approximation of absolute error $\tilde{A}$ & defect in range $p=10..100$ bar





Perspective: Linear Improvement of Theoretical Model with Empirical Model



Summary



Pro

- Less dependent on theoretical model in sensor front end
- Lowers number of iterations in model improvement
- Empirical model compensates for the complete error chain
- Extrapolation capability of empirical model can be scaled (exp. expense vs. extrapolation)
- Only one-time SW change (weights will be loaded)

Contra

- Hybrid model require capability and willingness to work abstractly on architecture level
- Significant change of theoretical model might require new experiments