
This item was submitted to [Loughborough's Research Repository](#) by the author.
Items in Figshare are protected by copyright, with all rights reserved, unless otherwise indicated.

Novel microstructured polyol-polystyrene composites for seasonal heat storage

PLEASE CITE THE PUBLISHED VERSION

<https://doi.org/10.1016/j.apenergy.2016.03.023>

PUBLISHER

© Elsevier

VERSION

AM (Accepted Manuscript)

PUBLISHER STATEMENT

This work is made available according to the conditions of the Creative Commons Attribution-NonCommercial-NoDerivatives 4.0 International (CC BY-NC-ND 4.0) licence. Full details of this licence are available at: <https://creativecommons.org/licenses/by-nc-nd/4.0/>

LICENCE

CC BY-NC-ND 4.0

REPOSITORY RECORD

Puupponen, Salla, Valtteri Mikkola, Tapio Ala-Nissila, and Ari Seppala. 2019. "Novel Microstructured Polyol-polystyrene Composites for Seasonal Heat Storage". figshare. <https://hdl.handle.net/2134/31890>.

ARTICLE

Novel microstructured polyol-polystyrene composites for seasonal heat storage

Cite this: DOI: 10.1039/x0xx00000x

Salla Puupponen,^{a†} Valtteri Mikkola,^a Ari Seppälä^a and Tapio Ala-Nissila^{b,c}

Received 00th January 2015,

Accepted 00th January 2015

DOI: 10.1039/x0xx00000x

www.rsc.org/

We propose a robust route to prepare supercooling microstructured phase change materials (PCMs) suitable for long-term heat storage or thermal protection applications. The new preparation method is based on polymerization of high internal phase emulsion (HIPE). Two promising polyols, erythritol and xylitol, are successfully prepared as new type microencapsulated PCM-polystyrene composites with PCM mass fractions of 62w-% and 67 w-%, respectively, and average void diameter of ~50 μm . Thermal properties of polyol-polystyrene composites and bulk polyols are studied thoroughly with differential scanning calorimetry (DSC). Microscale engineering has a significant impact on the thermal properties of polyols. Crystallization of the microscale erythritol is accelerated as compared to the crystallization of bulk PCM due to high fraction of solid surfaces in the polymer-polyol composites. Furthermore, crystallization properties of the microstructured erythritol are preserved similar in the cycling experiments. Crystallization of the bulk erythritol is found to strongly depend on the cooling rate, thermal history of the sample and surface roughness of the crucible, whereas these factors have only little impact on the crystallization of microstructured erythritol. In addition, microstructured polyol-polystyrene composites show anomalous enhancement in the specific heat as compared to bulk polyols. This enhancement may be originated from the strong polyol-surfactant interactions occurring in the composites.

1. Introduction

Growing energy consumption requires development of more efficient ways to produce and use energy than available to date. High efficiency energy storage technology would greatly improve the effectiveness of intermittent energy conversion technologies and facilitate inconstant energy use. During the last decades, researchers have started to realise the potential of phase change materials (PCMs) as thermal energy storage (TES) materials due to their greater heat storage density as compared to traditional 'sensible' heat storages. By far the most researched PCMs are chemically stable nonpolar paraffins and fatty acids with moderate heats of fusion. These standard PCMs release the heat stored when the temperature decreases below the thermodynamic equilibrium phase change temperature (T_{eq}) during solidification. Thus, these PCMs operate as 'thermal buffers' in short-term heat storages.¹⁻³

Supercooling of many promising PCMs, such as salt hydrates and sugar alcohols, is considered to be the main disadvantage hindering their use in TES. However, supercooling could actually be utilized in seasonal heat storages. In this case, the heat could be stored in the supercooled liquid for an unlimited time at temperatures substantially lower to T_{eq} and released by crystallization when the supplement heat is required. However, the metastable nature of supercooling liquids introduces some problems to the utilization of the phenomenon; the crystallization is not well controlled in the supercooled state and may be initiated spontaneously without any

external interference. In addition, the slow speed of the crystallization front at the recalescence for macroscale volumes can be a major obstacle for reaching thermally efficient storage process.

The problems related to crystallization of supercooling PCMs may be solved by micro- or nanoscale engineering. Distribution of the material into large number of microscale units greatly enhances the efficiency of solidification.⁴ In addition uncontrollable, spontaneous crystallization of supercooled liquid is avoided as PCM is divided into separate microscale cells by introducing discontinuities into the crystallized material.^{5,6}

Only a few studies to date have addressed the micro- or nanostructuring of supercooling PCMs. Sagara *et al.*⁵ studied the thermal properties of D-mannitol impregnated into nanosized silica pores, and Salaün *et al.*^{6,7} researched microencapsulation of sodium phosphate dodecahydrate (DSP) and xylitol using interfacial polymerization of poly(urea-urethane) films as encapsulating agent. The chemical structures of PCM microparticles were extensively examined in the studies^{6,7}, but the melting and crystallization properties of the PCMs were not studied. The main finding of the study of Sagara *et al.*⁵ was that nanoengineering facilitated thermal endurance, but simultaneously the melting heat of the PCM greatly decreased.

Here, we propose a novel and unique route to prepare microstructured polyols. Two promising supercooling polyols;

xylitol and erythritol, are chosen as model PCMs in this study. The new preparation method utilizes the polymerization of high internal phase emulsions (HIPEs) used generally for preparation of polymeric foams.⁸⁻¹⁰ By this new procedure, a large fraction of polyol can be captured inside micro-pores of polymer matrix in a robust manner. In addition to TES, the proposed PCM-crosslinked polystyrene composites could be promising thermal protection candidates, as a heat storage material and polystyrene with a low thermal conductivity are combined in the structure.^{11,12} Polymerization of HIPEs has previously been utilized for developing toner particles for electrophotographic printing.^{13,14} However, this technology has not been applied earlier to development of heat storage materials. In addition, thermal properties of the bulk and microscale polyols are extensively characterized here using differential scanning calorimetry (DSC). We focus particularly on the crystallization of supercooling PCMs that, in general, is only briefly reported in the literature.

2. Experimental section

Materials and preparation methods

Styrene (assay \geq 99%) and divinylbenzene (60-65 area%, ethylvinylbenzene 34-39 area% by GC) were supplied by Merck. Sorbitan monooleate (Span80, synthesis quality) from Merck was chosen for surfactant due to its optimal hydrophilic-lipophilic balance (HLB) of 4.3 for emulsification of water-in-oil system.^{9,10} Two radical initiators, polar potassium persulfate (KPS) from VWR and nonpolar azobisisobutyronitrile (AIBN) from Sigma-Aldrich were used to initiate the polymerizations.

Preparation of polystyrene HIPE foams

Polystyrene foams were prepared by polymerization of high internal phase emulsions. Conventional polymerized high internal phase emulsions (HIPEs) are microcellular foams produced typically by emulsification of water - hydrophobic monomer - hydrophobic surfactant tricomponent system, after which the continuous monomer phase is polymerized in the presence of a crosslinker agent. In our study, the preparation parameters were optimized in order to obtain closed-cell foam for development of microstructured PCMs.

Organic phase was prepared by mixing appropriate amounts of sorbitan monooleate (SMO) and styrene (St) for \sim 5 min using a magnetic stirrer. In some samples, the crosslinker agent divinylbenzene (DVB) was added to the organic phase. If nonpolar AIBN was used as an initiator, it was also added to the organic phase. The monomers were used without removing the inhibitors. Aqueous phase was prepared by mixing an appropriate amount of de-ionized water and KPS, if used as an initiator, with magnetic stirrer for \sim 5 min. The total mass of the wet samples was 50 grams, and mass fraction of the initiator was 0.15 wt-% in the samples. All reagents were weighed using the Precisa 360EP Executive PRO analysis scale with repeatability of 0.02 mg.

Emulsions were formed by a slow addition of the aqueous phase to the organic phase using a separating funnel and magnetic stirring.

Addition rate of the aqueous phase was kept as low as possible; generally the addition was complete in 20-30 min depending on the amount of water in the sample. Vaporization of volatile monomers was avoided by covering the samples carefully. Mixing was continued for 5-10 min after addition of the aqueous solution until a homogeneous, generally thick emulsion was obtained. The samples were taken either without, after 30 s, or after 1.5 min of ultrasonic mixing. During the ultrasonic processing (400 W power with Hielscher UP400S) the emulsions were placed in \sim 10 °C water bath. The emulsions were polymerized in sealed glass bottles for 24 h at 60-70 °C in a ventilated oven. After polymerization, the caps were removed and water was vaporized from the foams by keeping the samples in the oven at 70-80 °C until the sample weight stabilized.

Preparation of polyol-polystyrene composites

Two polyols were studied as promising supercooling PCMs; powdered erythritol (food grade, Jungbunzlauer) and crystalline xylitol (food grade, Danisco.) Polyol-polystyrene composites were prepared by dissolving sugar alcohol at \sim 50 °C to water during \sim 10 min using magnetic stirring, after which the samples were prepared similarly as described earlier, with the exception that the erythritol sample was mixed at \sim 40 °C in order to prevent crystallization of the highly supersaturated erythritol-water solution during emulsification. Maximum amounts of polyols that could be dissolved in the aqueous phase without crystallization during emulsification were 70 and 60 wt-% of the aqueous phase mass for xylitol and erythritol, respectively. The sample compositions are presented in Table 1.

Analysis methods

Foam structures were determined with optical microscopy (Leica Polarized Optical Microscope) in transmitting mode. The structures of polyol-polystyrene composites were imaged using incident light due to opacity of the composites. Thin pieces of samples were cut with a sharp blade for microscopy imaging. Thermal properties of polyol-polystyrene composites and bulk PCMs were measured with Netzsch DSC204FI Phoenix differential scanning calorimeter. Onset temperatures and latent heats were determined with accuracies of \pm 0.5 K and $<$ 1 %, respectively. The samples (10-20 mg) were hermetically sealed into aluminium crucibles. Three to six parallel measurements were conducted from each sample in order to obtain representative results. Two crucibles with different surface roughnesses, presented in Fig. 1., and a temperature range from -30 to 140 °C were used. In addition, preliminary crystallization tests of xylitol were conducted by cooling the samples to at most -50 °C and held there overnight. Two scanning rates of 0.5 and 5 K/min were used for studying the melting/crystallization kinetics and five to ten sequential phase change cycles were used for investigating the repeatability of melting/solidification. Specific heats of the samples were determined using a 5 K/min scanning rate. Stability of the supercooled state was assessed for few bulk and microstructured erythritol samples using a five hour long holding period at 50 °C, 5 K/min scanning rate and a crucible with a smooth surface. No crystallization was observed during these holding periods.



Fig. 1. Optical microscopy images of crucibles used in the DSC experiments. Left: crucible with a rough surface, right: crucible with a smooth surface. The scale bar (100 μm) is the same the in both images.

Table 1. Sample compositions. Abbreviations: AIBN – azobisisobutyronitrile, DVB – divinylbenzene, HIPE-ery – erythritol filled HIPE, HIPE-xyl – xylitol filled HIPE, KPS- potassium persulfate, SMO – sorbitan monooleate

Sample name	polyol/aqueous phase (wt-%)	aqueous phase (wt-%)	SMO/organic phase (wt-%)	DVB/organic phase (wt-%)	Initiator
HIPE-1	-	60	7	0	AIBN
HIPE-2	-	70	7	0	AIBN
HIPE-3	-	80	7	0	AIBN
HIPE-4	-	90	7	0	AIBN
HIPE-5	-	70	3	0	KPS
HIPE-6	-	70	5	0	KPS
HIPE-7	-	70	7	0	KPS
HIPE-8	-	70	9	0	KPS
HIPE-9	-	70	15	0	KPS
HIPE-10	-	70	5	5	KPS
HIPE-11	-	70	5	10	KPS
HIPE-12	-	70	5	20	KPS
HIPE-13	-	70	5	30	KPS
HIPE-14	-	70	5	40	KPS
HIPE-ery	60	74.3	5	30	KPS
HIPE-xyl	70	73.4	5	30	KPS

3. Results and discussion

Optimization of the polystyrene foam structure

Influence of the amount of the aqueous phase, initiator type, surfactant concentration and length and intensity of mixing on the foam structure were studied.

The impact of the amount of the aqueous phase on the foam structure was tested by varying the aqueous phase in the emulsion from 60 to 90 wt-%. Samples containing 70 or 80 wt-% aqueous phase produced the most stable emulsions that did not collapse during the water vaporization. A smaller amount of water (60 wt-%) produced inhomogeneous foam with hard bulk-polystyrene phase on top, whereas a sample with 90 wt-% of water did not produce an emulsion at all. Therefore, 70 and 80 wt-% emulsions were chosen for further studying.

Two radical initiators, nonpolar AIBN and polar KPS, were tested for polymerization initiation. No significant differences between the initiators were observed, but KPS initiated samples seemed to be more homogeneous and thus, KPS was chosen for further sample preparation. Ionic KPS initiates the polymerization from the styrene-water interface, whereas nonpolar AIBN initiates the polymerization randomly from the bulk styrene. Quick solidification of the oil-water interfaces may enhance the emulsion stability by preventing rapidly the coalescence of dispersed aqueous droplets.

Surfactant concentration impacts greatly on the foam structure as presented in Fig. 2. Foams with closed-cell pores were obtained with SMO/organic phase ratio of 5 wt-%. Emulsion did not form altogether with lower SMO/organic phase ratio of 3 wt-%, whereas slightly higher surfactant concentration of 7 wt-% resulted in formation of small windows between the micropores.

The micropores were strongly interconnected when SMO/organic phase ratio was increased further to 9 and 15 wt-%. Williams and Wroblewski⁹ proposed that small amount of surfactant results in completely closed water droplets due to formation of a thin, monomolecular surfactant layer on the droplet surfaces. As the amount of surfactant increases the polymer wall between water droplets becomes thinner as the hydrophobic surfactant molecules penetrate deeper into the organic phase creating small passages between the water droplets. Since closed-cell structure was desired for creation of microstructured PCMs, SMO/organic phase ratio of 5 wt-% was selected for further preparation. Two aqueous phase fractions, 70 and 80 wt-% were tested using this surfactant concentration. Closed-cell structure with 80 wt-% of water was extremely difficult to produce, and thus other samples were prepared with 70 wt-% aqueous phase amount.

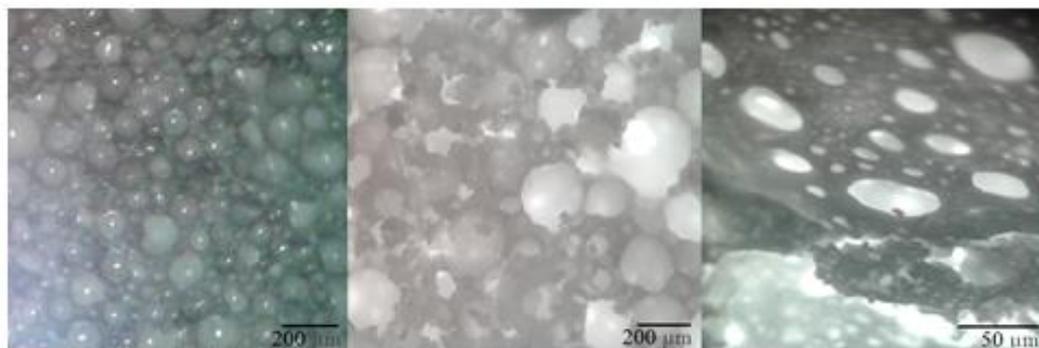


Fig. 2. Optical microscopy images of foam samples with different SMO/organic phase ratios. Left: HIPE-6 (5 wt-% SMO/organic phase), middle: HIPE-7 (7 wt-% SMO/St), right: HIPE-9 (15 wt-% SMO/St.)

Divinylbenzene stabilizes the foam system by crosslinking the polystyrene chains quickly together during polymerization.^{9,10} The influence of DVB concentration on the cell structure was tested by varying the DVB weight fraction between 5 and 40 wt-% in the organic phase. All foam samples containing DVB were relatively stable and demonstrated no or little collapse during vaporization of water. It was found out that increasing DVB resulted in slight decrease in void size and - distribution. Simultaneously, the emulsion softness increased.

The void sizes and void size distributions were found to decrease as the DVB concentration increased from 10 to 30 wt-% in the organic phase. HIPE-10 sample with 5 wt-% of DVB had relatively narrow void size distribution with an average void size of ~200 µm, but was extremely brittle. HIPE-11 and HIPE-12 samples containing 10 and 20 wt-% DVB in the organic phase had a wide distribution of void sizes; most of them were relatively small (10-40 µm) but also several larger voids (80-120 µm) could be observed. HIPE-13 containing 30 wt-% DVB in the organic phase had a narrower size distribution with an average pore size of ~40 µm. In addition, the mechanical properties of HIPE-13 were good; the foam was hard but not brittle. When DVB concentration was further increased to 40 wt-% in the organic phase, the emulsion softness significantly increased destroying the emulsion stability. Therefore, DVB fraction of 30 wt-% of the organic phase was chosen for further preparation. The average void sizes of the samples were determined by calculating the mean average of ~50 voids.

The effect of mixing was tested by mixing the emulsions in three different ways. The emulsions were first formed as in the conventional HIPE method using only magnetic stirring and slow addition rate of the aqueous phase.⁸⁻¹⁰ Part of the emulsion was further emulsified ultrasonically and the samples were taken after ~30 s and ~1.5 min mixing times. Generally, a short ultrasonic processing of ~30 s increased the emulsion viscosity and thus the emulsion stability, whereas longer mixing of ~1.5 min destroyed the emulsion structure. The degradation was noticed by an abrupt decrease in the emulsion viscosity after ~1 min ultrasonic processing.

These impacts can be understood by the ultrasound's ability to both initiate polymerization and cause depolymerization.

Ultrasonic processing may initiate the polymerization of vinylic groups alone¹⁵⁻¹⁷ or accelerate the homolytic fission of chemical initiators due to extremely high local temperatures in the vicinity of collapsing bubbles.¹⁸⁻²⁰ In addition, ultrasonic cavitation causes degassing resulting in depletion of oxygen that enhances the polymerization by preventing chain transfer reactions. Ultrasonic treatment may also cause polymer degradation due to possible cleavage of polymeric chains in violent mixing conditions.^{19,21,22} The origin of this effect is still under some debate, but cavitation occurring during high intensity mixing has shown to have a significant impact on degradation. This effect has been observed to be relatively independent on the chemistry of the polymer, but rather depend on the polymer chain length. Degradation has been reported to propagate faster for low molecule weight polymers at low temperatures and dilute solutions, as in the case of emulsions studied.¹⁹

Polyol-polystyrene composite structures

Solubility of polyols and densities of polyol – water solutions are important factors in successful preparation of polyol – polystyrene composites. The higher the solubility the more PCM can in principle be engaged into the HIPE structure. Xylitol is highly soluble in water (~62 g/100 g H₂O at 20 °C), whereas the solubility of erythritol is poorer (~32 g/100 g H₂O at 20 °C.) However, the solubility of erythritol increases substantially at higher temperatures, being ~78g/100g H₂O at 80 °C. The solubility of xylitol is ~93g/100g H₂O at 80 °C.

The maximum polyol fractions in the aqueous phase that maintained stable liquids during emulsification without crystallization were 60 and 70 wt-% for erythritol and xylitol, respectively. In the preparation of erythritol filled HIPE, temperature was kept at ~40 °C during emulsification in order to prevent crystallization of the highly supersaturated polyol solution.

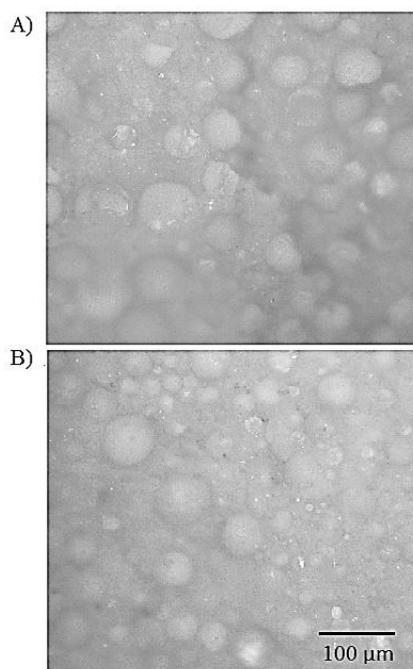


Fig. 3. Optical microscopy images of polyol-polystyrene composites: A) xylitol filled HIPE (HIPE-xyl) and B) erythritol filled HIPE (HIPE-ery). The scale bar (100 μm) is same in both images.

It has to be acknowledged that when the system is emulsified at elevated temperatures, polymerization may start already in the mixing stage. However, no significant changes in the appearance of the erythritol sample were observed as compared to other samples produced at 10 $^{\circ}\text{C}$. Densities of the solutions significantly influence the stability of emulsions; dissolution of polyols notably increases the density of the aqueous phase causing destruction of the emulsion structure due to density differences between the organic and aqueous phases. The organic phase density used for preparation of polyol – polystyrene composites (30 wt-% DVB, 5wt-% SMO and 65 wt-% St) was ~ 0.91 g/ml, whereas the densities of 60 wt-% erythritol- and 70 wt-% xylitol-water solutions were ~ 1.24 g/ml and ~ 1.25 g/ml, respectively. Therefore, the densities of polyol-water solutions were $\sim 35\%$ higher than that of the organic phase.

The best polyol filled foams were obtained when the emulsions were mixed 30 s - 1.5 min ultrasonically. The instability of emulsions formed by magnetic stirring only may be understood by a rapid phase separation due to the great density differences. Ultrasonic processing initiates polymerization when the continuous phase begins to solidify preventing the sedimentation of dense aqueous phase.

Optical microscopy images of the polyol-polystyrene samples are presented in Fig. 3. The average void sizes of xylitol and erythritol filled HIPEs were ~ 60 μm and ~ 40 μm , respectively. The void sizes of both samples varied between 15-90 μm indicating relatively wide pore size distribution typical for emulsions mixed mechanically.³⁰

Thermal properties of erythritol and erythritol-polystyrene composite

Erythritol crystallizes spontaneously when sufficiently cooled²³⁻²⁵, whereas many other polyols, such as xylitol, are remarkably stable in the supercooled state and thus are difficult to crystallize spontaneously only by cooling the sample.^{26,27} Lower supercooling degree of erythritol can be understood by similarities of the most stable crystalline and melt erythritol conformers; both possess straight backbone conformations.²³ Main thermal properties of bulk erythritol are presented in Table 2.

Table 2. Thermal properties of bulk erythritol. Abbreviations: T_{pc} – melting - / crystallization temperature, ΔH – latent heat of melting/crystallization. Repeatability of T_{pc} and ΔH are reported after the average values.

Measurement	T_{pc} ($^{\circ}\text{C}$)	ΔH (J/g)
<i>Melting (smooth crucible)</i>		
0.5 K/min	119 \pm 1	329 \pm 14
5 K/min	116 \pm 1	319 \pm 20
<i>Crystallization (smooth crucible)</i>		
0.5 K/min	25 \pm 28	-204 \pm 26
5 K/min	22 \pm 31	-101 \pm 65
<i>Crystallization (rough crucible)</i>		
0.5 K/min	52 \pm 30	-204 \pm 25
5 K/min	24 \pm 20	-203 \pm 20

The average melting temperature and melting heat of bulk erythritol were ~ 118 $^{\circ}\text{C}$ and ~ 324 J/g, respectively, being consistent with the values reported for pure erythritol in the literature (117-118 $^{\circ}\text{C}$ and 319-323 J/g).^{25,28,29} The melting temperature and melting heat remained constant between parallel measurements and sequential melting-crystallization cycles, albeit the melting heat was slightly higher when the lower heating rate of 0.5 K/min was used. The endpoint of the melting was ~ 135 $^{\circ}\text{C}$ despite the used heating rate.

The effect of surface roughness and cooling rate on the crystallization of bulk erythritol is shown in Fig. 4. Bulk erythritol crystallized rather coincidentally; the crystallization temperatures varied greatly between the parallel measurements and sequential melting-crystallization cycles. Crystallization may be induced by impurities as well as surface roughness of the crucible. Once the crystallization is induced, it progresses as a crystallization front through the whole bulk PCM.

The cooling rate of 5 K/min was observed to be inadequate due to the slow speed of crystallization front when a crucible with a smooth surface was used.

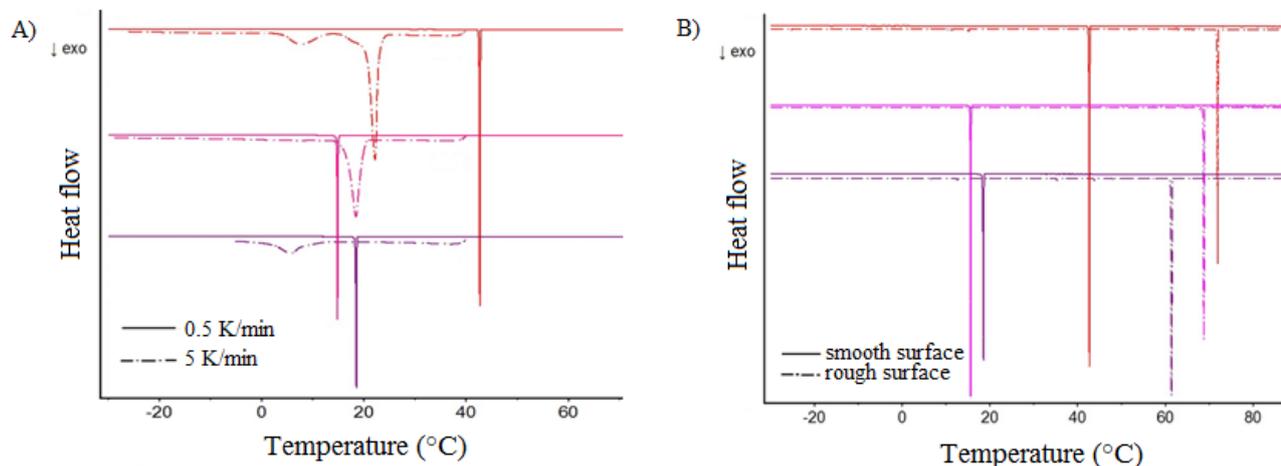


Fig. 4. Typical cooling DSC curves for bulk erythritol: A) Effect of the cooling rate and B) surface roughness on the crystallization. Superposed curves present sequential crystallization cycles

The smooth surface provides fewer nucleation sites, and therefore crystallization begins only from a few spots. In this case, the time scale in 5 K/min measurements is too short to allow complete crystallization. Upon complete crystallization, the absolute value of crystallization heat was ~ 200 J/g.

Furthermore, in some 5 K/min measurements, bulk erythritol did not crystallize until it was heated up again from -30 °C to -10 °C. This behavior was found to occur more often after several melting-crystallization cycles. In addition, occasionally a small exothermic peak was observed between -5 and 50 °C during heating indicating crystallization of conformer with smaller frequency of occurrence. Similar behavior has been reported earlier for pure erythritol.²⁴

Surface roughness had a great influence on the crystallization of bulk erythritol when a low cooling rate of 0.5 K/min was used. Indeed, the onset of crystallization increased on average from ~ 25 °C to ~ 52 °C when a rough surface crucible was used. The rough surface introduces nucleation sites particularly if the wetting between supercooled PCM and the crucible is sufficient resulting in decrease in supercooling. However, microstructure of the crystallization surface greatly affects the nucleation process; in some measurements the bulk erythritol crystallized at 60 – 70 °C in the sequential cycles, whereas in other cases the crystallization temperature varied between 15 – 40 °C. This effect was not observable when a higher cooling rate of 5K/min was used.

Main thermal properties of the erythritol-polystyrene composite are presented in Table 3.

Table 3. Thermal properties of the erythritol-polystyrene composite. Abbreviations: T_{pc} – melting/crystallization temperature, ΔH – latent heat of melting/crystallization. Repeatability of T_{pc} and ΔH are reported after the average values. $\Delta H_{meas.}/\Delta H_{calc.}$ – measured/calculated ΔH (cf. Eq. (1)) Latent heats are reported per total mass of the composite.

Measurement	T_{pc} (°C)	ΔH (J/g)	$\Delta H_{meas.}/\Delta H_{calc.}$
<i>Melting</i>			
<i>(smooth crucible)</i>			
0.5 K/min	110 ± 6	143 ± 4	0.71
5 K/min	110 ± 10	151 ± 20	0.77
<i>Crystallization</i>			
<i>(smooth crucible)</i>			
0.5 K/min	45 ± 4	-100 ± 5	0.80
5 K/min	32 ± 5	-86 ± 15	1.38
<i>Crystallization</i>			
<i>(rough crucible)</i>			
0.5 K/min	45 ± 2	-109 ± 10	0.87
5 K/min	40 ± 5	-92 ± 5	0.74

The average melting temperature of microstructured erythritol was ~ 7.5 °C lower than that of bulk erythritol. In addition, HIPE-ery melted at a wider temperature range than bulk erythritol indicating a broad void size distribution due to mechanical mixing in the emulsification.^{30,31}

If surface effects are ignored, the latent heat of polyol-polystyrene composite can be calculated from the mass fraction of the PCM in the product as:

$$\Delta H_{calc.} = \varphi \Delta H_{bulk} \quad (1)$$

where φ is the mass fraction of the polyol in the product and ΔH_{bulk} is the melting/crystallization heat of bulk polyol.

The measured melting heat of HIPE-ery was on average 74% of the theoretical one obtained from Equation (1). The lower melting heat and - temperature of nanomaterials is usually explained by the large fraction of a nonfreezing liquid layer in small-scale systems resulting in lower free energy.^{5,30} However, this effect should not be dominant in the microscale samples studied here, in which the surface area-to-volume ratio is substantially lower as compared to nanoscale systems.

The foam structure is likely to have a significant impact on the thermal properties of PCM in the composite. The void surfaces are surrounded by the surfactant molecules whose polar head groups penetrate inside the voids. The headgroup of SMO contains several hydroxyl groups resulting in strong interactions between the headgroups and the polyol molecules on the void surfaces. The filling fraction (estimated from the erythritol densities and the sample volume) of the composite is relatively low (54% and 47% for the melt and solid HIPE-ery, respectively) and thus, most of the voids are not completely filled with the polyol allowing large fraction of the PCM to occupy the surface positions where the strongest surfactant/polyol interactions occur. In addition, some erythritol molecules may migrate further into the foam structure during water vaporization enhancing the surfactant/polyol or polystyrene/polyol interactions. These interactions and possible distortions caused by them may largely determine the crystal structure of the microstructured erythritol, since the heterogeneous nucleation is likely to occur on the surfaces.

Influence of the cooling rate and surface roughness on the crystallization of microscale erythritol is presented in Fig. 5.

Crystallization of the erythritol-polystyrene composite seems substantially more reproducible than that of bulk erythritol. Indeed, the crystallization temperatures, heats and peak shapes of erythritol-polystyrene composite varied substantially less than those of the bulk erythritol.

The crystallization temperatures of HIPE-ery were between 41-49 °C and 27-45 °C when 0.5 and 5 K/min cooling rates were used, respectively. Therefore, the higher cooling rate slightly increased the supercooling degree of HIPE-ery. The crystallization heats were between 70-105 J/g with both cooling rates, lying in a narrower range than in the case of bulk PCM. The measured crystallization heat is ~20 % lower (0.5 K/min) than the calculated value obtained from Equation (1).

The crystallization heats of both bulk and microstructured erythritol samples were substantially lower than the corresponding melting heats. The crystallization heat reduction can be explained by the large supercooling degree of erythritol and differences in the specific heats of solid and liquid PCM:

$$\Delta H_{T_m} - \Delta H_{T_{cryst.}} = \int_{T_{cryst.}}^{T_m} (c_{p,liquid} - c_{p,solid}) dT \quad (2)$$

where T_m is the melting temperature, $T_{cryst.}$ is the crystallization temperature, ΔH_{T_m} and $\Delta H_{T_{cryst.}}$ are the latent heats in T_m and $T_{cryst.}$, respectively, and $c_{p,liquid}$ and $c_{p,solid}$ are the specific heats of liquid and solid PCM, respectively.

Values used for determination of crystallization heat reduction in the erythritol samples are presented in Table 4. The specific heats of erythritol samples and comparison of measured and calculated crystallization heat of bulk erythritol as a function of temperature are showed in Fig. 6.

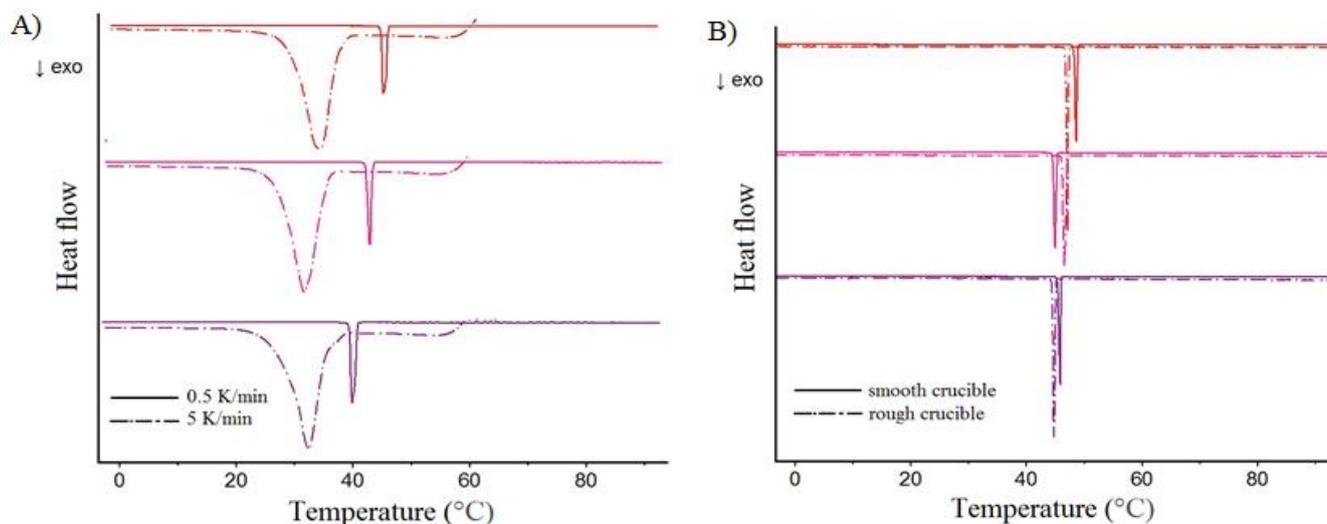


Fig. 5. Typical cooling DSC curves for erythritol-polystyrene composite: A) Effect of cooling rate and B) surface roughness on crystallization. Superposed curves present sequential crystallization cycles

Table 4. Crystallization heat reduction of the erythritol samples. Abbreviations: $c_{p,solid}$ – specific heat of solid PCM, $c_{p,liquid}$ – specific heat of liquid PCM, T_m – melting temperature, $T_{cryst.}$ – crystallization temperature, $\Delta H_{T_m} - \Delta H_{T_{cryst.}}$ – difference in latent heats at T_m and $T_{cryst.}$, $\Delta H_{meas.,cryst.}$ – measured crystallization heat, $\Delta H_{calc.,cryst.}$ – calculated crystallization heat (cf. Eq (2).) Specific heats are tabulated at 40 °C, T_m , $T_{cryst.}$ and $\Delta H_{meas.,cryst.}$ are the average measured values (0.5 K/min, smooth surface crucible)

Sample	$c_{p,solid}$ (J/gK)	$c_{p,liquid}$ (J/gK)	T_m (°C)	$T_{cryst.}$ (°C)	$\Delta H_{T_m} - \Delta H_{T_{cryst.}}$ (J/g)	$\Delta H_{calc.,cryst.}$ (J/g)	$\Delta H_{meas.,cryst.}$ (J/g)
bulk erythritol	1.42	2.51	119	25	-100.7	-219.2	-204±26
HIPE-ery	2.02	2.72	110	45	-68.6	-82.4	-100±5

Specific heats of solid and liquid erythritol samples differ greatly from each other, giving rise to the crystallization heat reduction observed in the measurements. Peculiarly, the specific heat of HIPE-ery was larger than that of bulk erythritol despite the lower specific heat of polystyrene foam ($c_{p,HIPE-13 \text{ foam}} = 1.31 \text{ J/gK}$ at 40 °C). The specific heat of HIPE-ery is larger both in solid and liquid state of PCM, but is more significant in the solid state. This anomalous behavior may originate from the strong hydrogen bonding between SMO and PCM molecules in the voids; the erythritol molecules may possess extensive hydrogen bonding, which is manifest in the enhanced specific heat.

Average supercooling degree and the difference in specific heats of bulk erythritol in solid and liquid state are larger (94 °C and 1.12 J/gK) as compared to the values of HIPE-ery (65 °C and 0.80 J/gK), causing together the greater crystallization heat reduction of bulk erythritol. However, the crystallization heat reduction strongly depends on the crystallization temperature as presented in Fig. 5B. The measured crystallization heat follows the calculated one relatively well at a temperature range of 30-50 °C, but decreases with smaller supercooling degrees. This behavior may originate from the slower speed of crystallization front due to higher viscosity of the supercooled liquid at lower temperatures, resulting in incomplete crystallization of the highly supercooled erythritol.

Thermal properties of xylitol and xylitol-polystyrene composite

Xylitol supercools easily and may retain the supercooled state for a long period of time.²⁷ Neither the studied bulk xylitol nor the xylitol-polystyrene composite crystallized spontaneously only by cooling the sample at most to -50 °C in the DSC experiments. Therefore, only the first melting peak of the PCM was observed in the measurements. Table 5 summarizes the thermal properties of the xylitol samples.

Melting properties of HIPE-xyl were similar than those of HIPE-ery. The melting temperature of HIPE-xyl was ~15 °C lower than that of bulk xylitol. In addition, xylitol-polystyrene composite melted at a wider temperature range than bulk xylitol as in the case of microstructured erythritol. The measured melting heat of HIPE-xyl was 100-125 J/g, being ~70% of the calculated one obtained from Equation (1) and corresponding well to the melting heat of HIPE-ery. The results of xylitol samples are only suggestive since the values present only the first melting cycle that may differ from subsequent phase change properties due to major changes occurring in the PCM microstructure during first melting cycle.

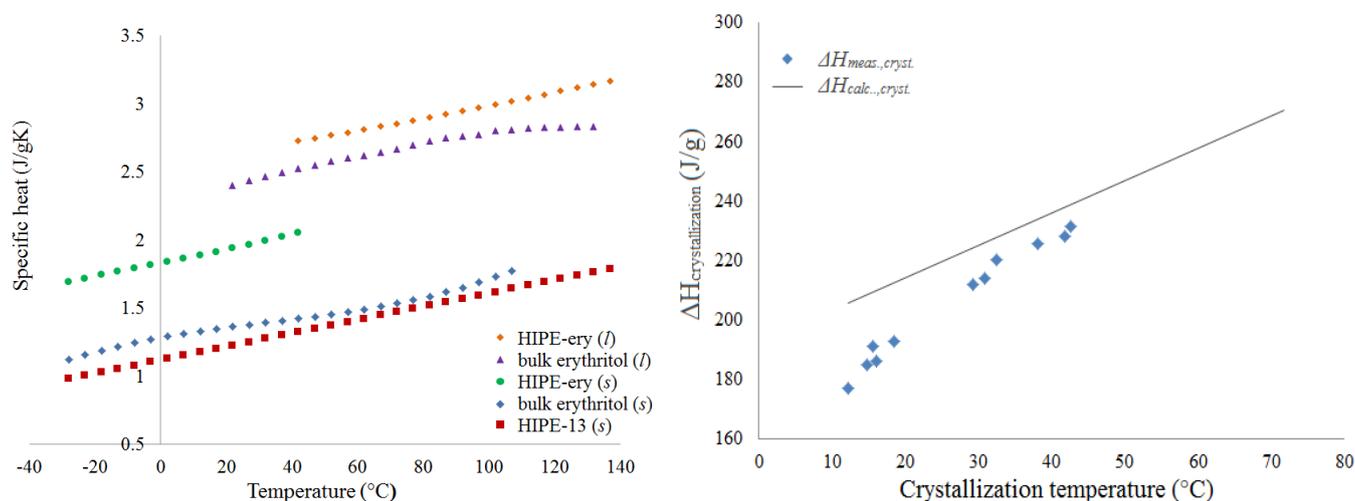


Fig. 6. A) Specific heats of bulk erythritol, HIPE-ery and HIPE-13 foam as a function of temperature. Phases of the samples (solid, *s* or liquid, *l*) are presented in the legends. Specific heat of HIPE-ery is presented per total mass of the sample. B) Comparison of measured and calculated crystallization heats of bulk erythritol as a function of crystallization temperature

Table 5. Melting properties of bulk xylitol and xylitol-polystyrene composite. Abbreviations: T_m – extrapolated onset melting temperature, ΔH_m – average melting heat, $\Delta H_{meas.}/\Delta H_{calc.}$ – measured / calculated ΔH_m of HIPE-xyl (cf. Eq. (1)). Latent heats are reported per total mass of the samples.

Sample	T_m (°C)	ΔH_m (J/g)	$\Delta H_{meas.}/\Delta H_{calc.}$
<i>Bulk xylitol</i>			
0.5 K/min	93±1	236±4	-
5 K/min	93±1	241±2	-
<i>HIPE-xyl</i>			
0.5 K/min	80±5	110±10	0.70
5 K/min	81±5	115±10	0.71

The specific heats of bulk xylitol, xylitol-polystyrene composite and HIPE-13 foam as a function of temperature are shown in Fig. 6.

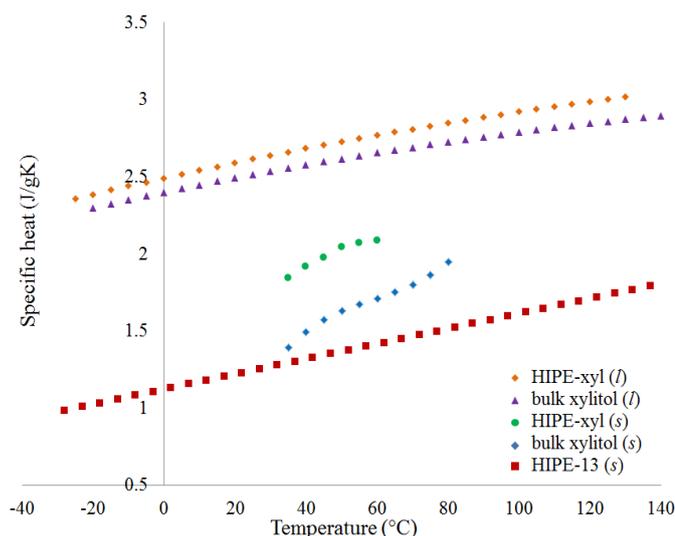


Fig. 6. Specific heats of bulk xylitol, HIPE-xyl and HIPE-13 foam as a function of temperature. Phases of the samples (solid, *s* or liquid, *l*) are presented in the legends. Specific heat of HIPE-xyl is presented per total mass of the sample.

The specific heats of bulk xylitol and HIPE-xyl demonstrated similar behavior than in the case of erythritol samples; in both cases polyol-polystyrene composites showed enhanced specific heat as compared to the specific heats of bulk PCMs and HIPE foam. The specific heat increase is more profound in the solid state; $c_{p,HIPE-xyl}/c_{p,bulk} = 1.31$ (solid state, 40 °C) and $c_{p,HIPE-xyl}/c_{p,bulk} = 1.04$ (liquid state, 40 °C).

4. Conclusions

We have demonstrated a novel, robust route to prepare microstructured PCMs based on the polymerization of high internal phase emulsions. Two supercooling polyols, xylitol and erythritol, were chosen as model PCMs for this study. Preparation parameters were optimized in order to obtain closed-cell foam structure with as small pore size and narrow pore size distribution as possible. The

surfactant fraction had strongest influence on the formation of the foam structure and the crosslinker agent significantly enhanced the foam stability. The optimal ratios of SMO and DVB to the organic phase were found to be 5 and 30 wt-%, respectively. The aqueous phase fraction was retained relatively low at 70 wt-%, as stable and closed-cell polymeric foam was desired for development of microstructured PCMs.

Polyol-polystyrene composites were obtained by dissolving polyols into water after which the emulsion was formed, styrene-DVB matrix polymerized, and water vaporized. The maximum erythritol and xylitol fractions that could be engaged into the foam structure were 62 wt-% and 67 wt-% of the dry product weight, respectively. The void sizes of the polyol-polystyrene composites were $50\mu\text{m} \pm 40\mu\text{m}$.

Thermal properties of the novel microscale polyols were studied thoroughly by DSC and compared to the properties of bulk polyols. Microscale engineering was found have a strong influence on the thermal properties of the polyols studied here. The supercooling degree, melting heat, and melting temperature of microstructured erythritol were lower than those of bulk erythritol. Similar melting properties were observed for the microscale xylitol sample. The highly supercooled xylitol samples maintained as liquids in the studied conditions ($T \geq -50$ °C) and thus, the crystallization properties of xylitol samples could not be studied.

The crystallization of microstructured and bulk erythritol differed greatly from each other. The erythritol-polystyrene composite crystallized in more controlled manner than the bulk erythritol; the crystallization heats and temperatures of microscale erythritol varied substantially less.

In addition to phase change characteristics, the specific heats of the polyol samples were studied with DSC. Peculiarly, the specific heats of both microscale erythritol and xylitol samples were higher than those of bulk PCMs ($c_{p,HIPE-ery}/c_{p,bulk} = 1.42$ and $c_{p,HIPE-xyl}/c_{p,bulk} = 1.31$ at 40 °C, solid state) despite the lower specific heat of the polystyrene foam. It is likely that strong SMO-polyol interactions give rise to enhanced hydrogen bonding in the microstructured polyol systems, resulting in larger specific heat of the HIPE samples.

Due to the substantial differences between the solid and liquid state specific heats and large supercooling degree of both erythritol samples, the crystallization heats of the samples were reduced as compared to the melting heats. For thermal energy storage, this reduction is clearly an undesired feature, and thus PCMs with smaller difference in $c_{p,s}$ should be discovered. In addition, the heat storing potential of microstructured PCMs should be increased for TES. Higher heat storing potential of the composites could possibly be reached if the density and solubility inflicted problems in the emulsions preparation could be solved, in which case higher fraction of PCM could be engaged into the foam.

However, the polyol-polystyrene-composites proposed here are extremely interesting for further studies of heat storage purposes due to their more effective solidification and more reproducible phase change characteristics as compared to bulk polyols. In addition, high specific heats of the composites combined with the heat storing and insulative properties of polyols and polystyrene matrix, respectively,

could make the proposed PCM-polystyrene composites attractive for heat or cold protection applications.

Acknowledgements

This work was carried out in the Efficient Energy Use (EFEU) research program coordinated by CLEEN Ltd. with funding from the Finnish Funding Agency for Technology and Innovation, Tekes, Fortum Foundation, Aalto Energy Efficiency Research Programme (EXPECTS-project) and supported in part by the Academy of Finland through its COMP CoE grant #251748.

Notes and references

^a Aalto University School of Engineering, Department of Energy Technology, P.O. Box 14400, FIN-00076 Aalto, Espoo, Finland

^b Aalto University School of Science, Department of Applied Physics and COMP CoE, P.O. Box 11000, FIN-00076 Aalto, Espoo, Finland

^c Brown University, Department of Physics, P.O. Box 1843, Providence, RI 02912, USA

† Corresponding author: Salla Puupponen: e-mail salla.puupponen@aalto.fi / tel. +358407277756

- 1 M. M. Farid, A. M. Khudhair, S. A. K. Razack, S. Al-Hallaj, *Energ. Convers. Manage.*, 2004, **49**, 1597-1615.
- 2 A. Sharma, V. V. Tyagi, C. R. Chen, D. Buddhi, *Renewable Sustainable Energ. Rev.*, 2009, **13**, 318-345.
- 3 B. Zalba, J. M. Marín, L. F. Cabeza, H. Mehling, *Appl. Therm. Eng.*, 2003, **23**, 251-283.
- 4 A. Seppälä, *Int. J. Heat Mass Tran.*, 2012, **55**, 1582-1595.
- 5 A. Sagara, T. Nomura, M. Tsubota, N. Okinaka, T. Akiyama, *Mater. Chem. Phys.*, 2014, **146**, 253-260.
- 6 F. Salaün, E. Devaux, S. Bourbigot, P. Rumeau, *Carbohydr. Polym.*, 2008, **73**, 231-240.
- 7 F. Salaün, G. Bedek, E. Devaux, D. Dupont, L. Gengembre, *J. Membr. Sci.*, 2011, **370**, 23-33.
- 8 D. Barby Z. Haq, U.S. Patent, 4,522,953 (Unilever applicant) Juny 11, 1985.
- 9 J. M. Williams, D. A. Wroblewski, *Langmuir*, 1988, **4**, 656-662.
- 10 J. M. Williams, A. J. Gray, M. H. Wilkerson, *Langmuir*, 1990, **6**, 437-444.
- 11 A. Seppälä, M. El Aj Hassad, T. Kapanen, *Struct. Multidisc. Optim.*, 2008, **36**, 355-363.
- 12 J. J. Zhang, Z. G. Qu, Z. G. Jin, *Energy*, 2014, **71**, 94-103.
- 13 D. P. Putnam, M. Nair, M. C. Brick, T. K. Jones, U.S. Patent, 8,252,414, August 28, 2012.
- 14 M. Nair, C. P. Lusignan, D. C. Boris, *Colloids Surf., A*, 2014, **443**, 583-595.
- 15 Y. He, Y. Cao, Y. Liu, *J. Polym. Sci., Part B: Polym. Phys.*, 2005, **43**, 2617-2624.
- 16 M. Bradely, F. Grieser, *J. Colloid Interface Sci.*, 2002, **251**, 78-84.
- 17 Y. Kojima, S. Koda, H. Nomura, *Ultrason. Sonochem.*, 2001, **8**, 75-79.
- 18 S. Biggs, F. Grieser, *Macromol.*, 1995, **28**, 4877-4882.
- 19 K. S. Suslick, G. J. Price, *Annu. Rev. Mater. Sci.*, 1999, **29**, 295-326.
- 20 A. S. Ostroski, R. B. Stambaugh, *J. Appl. Phys.*, 1950, **21**(478), 478-482.
- 21 G. Madras, S. Kumar, S. Chattopadhyay, *Polym. Degrad. Stab.*, 2000, **69**, 73-78.
- 22 H. W. Melville, A. J. R. Murray, *Trans. Faraday Soc.*, 1950, **46**, 996-1009.
- 23 J. S. Redinha, A. J. L. Jesus A. A. C. C. Pais, J. A. S. Almeida, in *Advanced Topics of Crystal Growth*, Intech, 2013, *Ch. 8*, pp. 201-224.
- 24 A. J. L. Jesus, S. C. C. Nunes, M. R. Silva, A. M. Beja, J. S. Redinha *Int. J. Pharm.*, 2010, **388**, 129-135.
- 25 R. A. Talja, Y. H. Roos, *Thermochim. Acta*, 2001, **380**, 109-121.
- 26 L. Carpentier, S. Desprez, M. Descamps, *J. Therm. Anal. Calorim.* 2003, **73**, 577-586.
- 27 A. Seppälä, A. Meriläinen, L. Wikstrom, P. Kauranen, *Exp. Therm. Fluid Sci.*, 2010, **34**(5), 523-527.
- 28 A. J. L. Jesus, L. I. N. Tomé, J. S. Redinha, M. E. Eusébio, *J. Phys. Chem. B*, 2005, **109**, 18055-18060.
- 29 G. Barone, G. D. Gatta, D. Ferro, V. Placente, *J. Chem. Soc., Faraday Trans.*, 1990, **86**(1), 75-79.
- 30 Q. Jing, M. D. Ward, *Chem. Soc. Rev.*, 2014, **43**, 2066-2079.
- 31 S. Puupponen, A. Seppälä, O. Vartia, K. Saari, T. Ala-Nissilä, *Thermochim. Acta*, 2015, **601**, 33-38.